CHAPTER 115
AIR EMISSION LICENSE APPLICATION FORMS

State of Maine
Department of Environmental Protection
Bureau of Air Quality
17 State House Station
Augusta, Maine 04333-0017
phone: (207) 287-2437 fax: (207) 287-7641

Revised 4/97

Section A: FACILITY INFORMATION

Facility Name to Appear on License: Irving Oil Terminals, Inc.
Emission Location: 52 Station Ave. City/Town: Searsport County: Waldo

Facility Contact: Drake Bell Title: Area Supervisor
Phone: 207-548-2541 Fax:

Facility Mailing Address: 52 Station Avenue
City/Town: Searsport, Me Zip Code: 04974
Facility Phone Number: 207-548-2541

Facility and Application Description:

SEE ATTACHMENT 1

Current License #: A- 413 - 71 - G - A
Application #: A- ____ - ____ - ____ - ____ (to be filled in by the Department)

Check When Done:

√ Application Completed
√ Copy Sent to Town (date sent Feb. 23, 2007)
√ Public Notice Published
(paper name: Waldo Independent date: (Feb. 10, 2007)
√ Enclosed Public Notice Tear Sheet
√ Signed Signatory Form (section J)
N/A If applicable, notified abutting landowners (major modification)
N/A If applicable, enclosed check for fee (new sources)

Section B: FUEL BURNING EQUIPMENT-With respect to Fuel Burning Equipment, no changes are proposed in this renewal licensing action.

Emission Unit #	Type of Equipment (boiler, furnace, engine, etc.	Maximum Design Capacity (MMBtu/hr)	Maximum Firing Rate (gal/hr)	Fuel Type (and % sulfur)	Date of Manufacture	Date of Installation	Stack #	Control Device
Boiler #1	Boiler	4.0	30	#6 at 0.20%	-	-	1	-
Boiler #2	Boiler	1.68	12	#2 at 0.35%	-	-	2	NA
Generator #1	Engine	0.7	7.4	Propane	-	-	-	-

Control Device Description for Fuel Burning Equipment-**Not Applicable**

Emission Unit #	Control Device	Pollutant(s) Controlled	Control Efficiency (%)

FUEL BURNING EQUIPMENT (section B cont'd)

Monitors for Fuel Burning Equipment: **Not Applicable**

If applicable, indicate types of required operated monitors, including CEM, COM, parameter monitors for operational purposes, etc.

Emission Unit #	Type of Monitor	Data Measured	Date Installed	Monitor Location

Section C: INCINERATORS Not Applicable

	Incinerator Unit 1	Incinerator Unit 2
Incinerator Type (medical waste, municipal, etc.)		
Date of Manufacture		
Date of Installation		
Number of Chambers		
Max. Design Feed Rate (per load)	lb	lb
Waste Type		
Max. Design Combustion Rate	lb/hr	lb/hr
Heat Recovery? (Yes or No)		
Retention Time	seconds	seconds
Automatic Feeder? (yes or No)		
Temperature Range primary	to °F	to °F
secondary	to °F	to °F
Auxiliary Burner - Primary Chamber max. rating (MMBtu/hr)		
type of fuel used		
Auxiliary Burner - Secondary Chamber max. rating (MMBtu/hr)		
type of fuel used		
Annual Waste Combusted for (yr)		
Pollution Control Equipment (if any)		
Stack Number		
Monitors (ie - temperature recorder)		

Section D: PROCESS EQUIPMENT

Emission Unit #	Type of Equipment	Maximum Raw Material Process Rate (name and rate)	Maximum Finished Material Process Rate (name and rate)	Date of Manufacture	Date of Installation	Stack #	Control Device
-	Loading Rack	411,850,701 gal/yr*		-	-	Fugitive	Carbon Adsorption

*** Refer to Table 4 located in Attachment 2, where 2005 loading rack throughput is broken down by product loaded at the rack.**

Control Device Descriptions for Process Equipment

Emission Unit #	Control Device	Pollutants(s) Controlled	Capture Efficiency (%)	Control Efficiency (%)
-	Carbon Adsorption Unit	VOC	0.9994 [1]	0.95

[1] Based on VOC Emission Test Report prepared on March 8, 2006 by The Jordan Service Company, Inc.

Associated Fuel Burning Equipment **Not Applicable**

Note: Complete this section for any fuel burning equipment integral to the process unit, ie. a dryer. Do not use this section for boilers or fuel burning equipment identified as a separate emission unit in Section B.

Emission Unit #	Type of Equipment	Maximum Input Rating (MMBtu/hr)	Maximum Firing Rate	Fuel Type incl. % Sulfur	Stack #

PROCESS EQUIPMENT (section D cont'd)

Associated Chemical Usage **Not Applicable**

Note: Complete this section for any chemicals integral to the process unit, for example, a cementing process for outersoles, dyes, surface coating, printing, cleaning, etc. Attach additional pages as needed.

Process	Chemical Compound Used in Process	Actual Compound Usage (gal or lb for yr _____)	Hazardous Chemical(s) in Compound	Percent VOC (%)	Percent HAP (%)	Total VOC Emitted (lb/year)*	Total HAP Emitted (lb/year)

Describe method of recordkeeping (ie. monthly calculations from purchase records, flow monitors on solvent tanks, etc.) _____

* Describe any assumptions used to calculate VOC emitted if 100% volatility is not used (ie - if control equipment was taken into account; if conditions exist where solvents remain in the substrate rather than complete volatilization, etc.)

_____

Section E: STACK DATA - Stack data remains unchanged since previous licensing action.

Stack #	Height Above Ground (circle units: m , ft)	Inside Diameter (circle units: , ft)	Exit Temperature °F	Flow Rate (m^3/s or ft^3/s) [indicate actual or standard]

Section F: ANNUAL FACILITY FUEL USE **Not Applicable**

Total Fuel Consumption by Month for: _____ (year)

	Fuel Use for Emission Units _____	Fuel Use for Emission Units _____	Fuel Use for Emission Units _____
	Avge % sulfur (oil) __ Avge % moisture (wood) ____ (circle one: gal, tons, scf)	Avge % sulfur (oil) __ Avge % moisture (wood) ____ (circle one: gal, tons, scf)	Avge % sulfur (oil) ____ Avge % moisture (wood) _ (circle one: gal, tons, scf)
January	_____	_____	_____
February	_____	_____	_____
March	_____	_____	_____
April	_____	_____	_____
May	_____	_____	_____
June	_____	_____	_____
July	_____	_____	_____
August	_____	_____	_____
September	_____	_____	_____
October	_____	_____	_____
November	_____	_____	_____
December	_____	_____	_____
Total	_____	_____	_____

Section G: LIQUID ORGANIC MATERIAL STORAGE - See Attachment 1 continuation of this table.

Emission Unit #	Tank 1	Tank 2	Tank 3	Tank 4[3]	Tank 5	Tank 6	Tank 7
Above or Below Ground	Above	Above	Above	Above	Above	Above	Above
Type (floating or fixed, riveted or bolted, etc.)	IFR[2]	IFR[2]	IFR[2]	VFR[1]	IFR[2]	IFR[2]	IFR[2]
Physical Description - age	-	-	-	-	-	-	-
Physical Description - color	White	Gray	White	Gray	White	White	White
Dimensions - height (ft)	48	48	48	48	48	48	56
Dimensions - diameter (ft)	162	162	110	162	110	137	132
Capacity (gallons)	7,350,000	7,350,000	3,360,000	7,350,000	3,360,000	5,250,000	5,670,000
Construction Type	Welded Steel	Welded Steel	Welded Steel	Welded Steel	Welded Steel	Welded Steel	Welded Steel
Materials Stored name	Gasoline	No. 2 Fuel	Kerosene	NA	Gasoline	No. 2 Fuel	Kerosene
vapor pressure & temp	3.5 - 6.9 psi @ 60° F	0.0074 @60° F	0.0085 psi @ 60° F	-	3.5 - 6.9 psi @ 60° F	0.0074 @60° F	0.0085 psi @ 60° F
RVP	7 - 13 psia	-	-	-	7 - 13 psia	-	-
total oxygen content	-	-	-	-	-	-	-
oxygenate name	-	-	-	-	-	-	-
annual throughput (gal.)	87,244,500	72,324,000	3,561,600	-	3,393,600	52,920,000	10,602,900
Loading (from trucks/ ships/barge, etc.)	Yes	Yes	Yes	Yes	Yes	Yes	Yes
Transferring (to truck/ to barge/to pipeline, etc.)	Yes	Yes	Yes	Yes	Yes	Yes	Yes
Control Device	Carbon Adsorption	Carbon Adsorption	Carbon Adsorption	No	Carbon Adsorption	Carbon Adsorption	Carbon Adsorption

[1] Vertical Fixed Roof (VFR)
[2] Internal Floating Roof (IFR)
[3] Not operational during 2005

NOTE: The information on the above table is based on 2005 operations. Products stored in the bulk storage tanks are subject to change based on market supply and demand. Tanks 14, 15, 21, 23, 24, 25, & 26 listed in existing license were noted for completeness only and remain unchanged. Tanks 16 and 17 are no longer in service at the terminal and can be removed from the license as a bulk storage source.

Section H: MISCELLANEOUS

Note: Use this section to describe any equipment, activities, or other air emission sources that did not fit in any of the above categories. Include descriptions of the associated emissions.
Equipment Description(s):

Section I: LIST OF ATTACHMENTS

Please Check the Appropriate Boxes Below

☐	Plot Plan	- Attachment NA
☐	Calculations	- Attachment 4
☐	BPT Analysis	- Attachment NA
☐	BACT Analysis (new sources)	- Attachment NA
☐	Schedule for Construction (new source, mod.)	- Attachment NA
☐	Title, Right, Interest Documentation (new source)	- Attachment NA
☐	MACT Demonstration	- Attachment NA
☐	Air Quality Modeling Analysis	- Attachment NA
☐	Ambient Air Monitoring Plan	- Attachment NA
☐	Stack Test Protocols/Reports	- Attachment NA
☐	Continuous Emissions	- Attachment NA
☐	Monitoring Plans/QA/QC	- Attachment NA
☐	Confidentiality Justification	- Attachment NA
☐	Operational Flexibility	- Attachment NA
☐	Description of Alternative Operating Scenarios	- Attachment NA
☑	Other Facility and Application Description	- Attachment 1
☑	Other 2005 Criteria Pollutant Emission Inventory and EPA "Tanks" Report	- Attachment 2
☑	Other Public Notice of Intent to File	- Attachment 3

Note: 'Other' documentation submitted may include identification of activities proposed as substantially equivalent to insignificant activities specified in Appendix B of Chapter 115; requests for specific requirements to be federally enforceable; etc.

Section J: SIGNATORY REQUIREMENT

Each application submitted to the Department must include the following certification signed by a Responsible Official:

"I certify under penalty of law that, based on information and belief formed after reasonable inquiry, I believe the information included in the attached document is true, complete, and accurate."

Drake Bell
Responsible Official Signature

9/21/06
Date

Drake Bell
Responsible Official (Printed or Typed)

Area Supervisor
Title

ATTACHMENT 1

FACILITY AND APPLICATION DESCRIPTION

The primary activities of Irving Oil Terminals, Inc. (Irving Oil), Searsport Terminal, includes the transfer (ship to shore), storage and distribution of refined petroleum products such as gasoline and distillate oils. General maintenance, cleaning and storage of facility owned tank trucks and other miscellaneous equipment also occurs at the site. The site is associated with 3 tank farms for the storage of petroleum products, Tank Farms #1, #2, and #3. Rail car and tank truck loading areas, office buildings, maintenance garage, and vehicle storage areas also exist at the site.

This application is for an Air Emission Renewal License for existing sources located at the Searsport Terminal. With the exception of Boiler #1, Emission sources at the facility have remained unchanged since their last Air Emission License Renewal (A-413-71-E-A/R) and License Amendment (A-413-71-G-A). Boiler #1 was originally licensed to burn #6 oil to provide tank and facility heating demands. The facility currently does not store #6 fuel oil and therefore is not utilizing this boiler. However, Irving Oil is proposing to keep Boiler #1 as an emission source in the event they begin accepting #6 oil in the future. Tanks 4 and 21 were previously used to store #6 fuel oil and will also remain as an emission source. Boiler #2 was added as an emission source as part of the Amendment discussed above and now provides for facility heating demands. Also added as an emission source as part of the above mentioned Amendment was a 70 kW propane fired generator to provide emergency electrical demand in the event of a power outage.

Continued from Section G: LIQUID ORGANIC MATERIAL STORAGE

Emission Unit #	Tank 8	Tank 9[3]	Tank 10[3]	Tank 11[3]	Tank 12[3]	Tank 13[3]	
Above or Below Ground	Above	Above	Above	Above	Above	Above	
Type (floating or fixed, riveted or bolted, etc.)	IFR[2]	VFR[1]	VFR[1]	VFR[1]	VFR[1]	VFR[1]	
Physical Description - age	-	-	-	-	-	-	
Physical Description - color	White	Gray	Gray	Gray	Gray	Gray	
Dimensions - height (ft)	56	40	40	40	40	40	
Dimensions - diameter (ft)	132	140	100	90	80	110	
Capacity (gallons)	5,670,000	4,620,000	2,100,000	1,680,000	756,000	2,100,000	
Construction Type	Welded Steel	Welded Steel	Welded Steel	Welded Steel	Welded Steel	Welded Steel	
Materials Stored name	No. 2 Fuel	NA	NA	NA	NA	NA	
vapor pressure & temp	0.0074 @60° F	-	-	-	-	-	
RVP	-	-	-	-	-	-	
total oxygen content	-	-	-	-	-	-	
oxygenate name	-	-	-	-	-	-	
annual throughput (gal.)	21,262,500	-	-	-	-	-	
Loading (from trucks/ ships/barge, etc.)	Yes	Yes	Yes	Yes	Yes	Yes	
Transferring (to truck/ to barge/to pipeline, etc.)	Yes	Yes	Yes	Yes	Yes	Yes	
Control Device	Carbon Adsorption	No	No	No	No	No	

[1] Vertical Fixed Roof (VFR)
[2] Internal Floating Roof (IFR)
[3] Not operational during 2005

NOTE: The information on the above table is based on 2004 operations. Products stored in the bulk storage tanks are subject to change based on market supply and demand.

ATTACHMENT 2

2005 CRITERIA POLLUTANT EMISSION INVENTORY AND EPA "TANKS" REPORT

JN: 4492

Table 1
Irving Oil Terminals, Inc.
2005 Criteria Pollutant Emission Summary

2005 Criteria Pollutant Emissions (Tons)						
Pollutant	**No. 6 Boiler**	**Storage Tanks**	**Loading**	**Equipment Leaks**	**Ballasting**	**Totals**
Carbon Monoxide (CO)	0.00	0.00	0.00	0.00	0.00	0.00
Sulfer Dioxide (SO_2)	0.00	0.00	0.00	0.00	0.00	0.00
Volatile Organic Compounds (VOCs)	0.00	8.56	5.65	0.10	0.00	14.31
Nitrogen Oxides (NO_X)	0.00	0.00	0.00	0.00	0.00	0.00
Fine Particulate Matter (PM2.5)	0.00	0.00	0.00	0.00	0.00	0.00
Fine Particulate Matter (PM10)	0.00	0.00	0.00	0.00	0.00	0.00
Ammonia (NH_3)	0.00	0.00	0.00	0.00	0.00	0.00

Table 2
Irving Oil Terminals, Inc.
2005 Criteria Pollutant Boiler Emission Summary

NOTE: The No. 6 fuel oil boiler was not utilized during 2005.

Table 3
Irving Oil Terminals, Inc.
2005 Storage Tank VOC Emissions

	Total VOC (lb)*			
Emission Source	**Gasoline**	**Jet/Kero**	**No. 6**	**No. 2/Diesel**
Tank 001.tn	9,793.98			
Tank 002				119.20
Tank 003		22.57		
Tank 004				
Tank 005.tn	6,288.41			
Tank 006.tn				91.42
Tank 007-A		27.13		
Tank 008-B				43.26
Tank 009				
Tank 010				
Tank 011				
Tank 012		0.00		
Tank 013				736.77
Total	16,082.39	49.70	0.00	990.65

*Based on AP-42 guidance VOC emissions average about 85 percent of total organic compound (TOC) emissions.

Total Storage Tank VOC = 17,122.74 lb

or

8.56 ton

NOTE: TOC Emissions were calculated using "Tanks 4.09" software.

Table 4
Irving Oil Terminals, Inc.
2005 Loading Loss VOC Emissions Calculations

Fuel Type	Loading Type	Percent of Thruput Loading Type is Used (%)*	Saturation Factor (S)	True Vapor Pressure of Liquid Loaded (psia)	Molecular Weight of Vapors (lb/lb-mole)	Average Temperature of Bulk Liquid (°R)	Collection Efficiency	Vapor Recovery Unit Efficiency	Tank Truck Loading Losses (lb/1000gal)	Thruput (gal/yr)	Total VOC Loading Loss Rate (Ton/yr)
Gasoline	Submerged Dedicated Vapor Balance	100	1	4.99	64.67	512.4	0.987	0.9979	0.118	90,628,091	5.36
Kero/Jet	Submerged Dedicated Vapor Balance	38.2	1	0.006675	130	512.4	0.987	0.9979	0.000	14,157,313	0.00
Kero/Jet	Splah Loading (Dedicated Normal Service	61.8	1.45	0.006675	130	512.4	0.987	0	0.031	14,157,313	0.13
No. 2/Diesel	Submerged Dedicated Vapor Balance	92.3	1	0.005283	130	512.4	0.987	0.9979	0.000	146,453,992	0.02
No. 2/Diesel	Splah Loading (Dedicated Normal Service	7.7	1.45	0.005283	130	512.4	0.987	0	0.024	146,453,992	0.14
No. 6	Splah Loading (Dedicated Normal Service	0	1.45	0.0000327	190	512.4	0.987	0	0.000	0	0.00
									Total VOC Losses		5.65

*Based on 2005 operations

The estimation method from AP-42 section 5.2.2.1.1 was used to determine tank truck loading losses for the year 2005.

The following equation was used to determine the losses:

$$L_L = 12.46 \times (SPM/T) \times (1\text{-eff.}/100)$$

Where:

L_L = Loading Loss, pounds per 1000 gallons (lb/10^3 gal) of liquid loaded

S = Saturation factor (AP-42 Table 5.2-1)

P = True vapor pressure of liquid loaded, pounds per square inch absolute (psia)

M = Molecular weight of vapors, pounds per pound-mole (lb/lb-mole)

T = Temperature of bulk liquid loaded (°R)

eff. = Efficiency of vapor control unit (*Collection Efficiency* x *Vapor Recovery Unit Efficiency*)

Table 5
Irving Oil Terminals, Inc.
2005 Equipment Leak VOC Emissions Calculations

Rack Lines							
Line Name	Fittings (Connectors and Flanges	Number of Pumps	Number of valves	Type of Fuel in Equipment	per Year Fuel Remains in equipment	Per Year Fuel Remains in Equipment	VOC Fuel Emission Rate (lb/yr)*
Tank 1	4	2	11	Gasoline	365	8760	7.24
Tank 2	1	0	3	No. 2	365	8760	2.25
Tank 3	4	1	8	Gasoline	365	8760	5.53
Tank 4	1	2	13	No. 6	0	0	0.00
Tank 5	4	1	11	Gasoline	365	8760	6.17
Tank 6	3	1	7	Kero	365	8760	14.20
Tank 7	0	0	0	Gasoline	365	8760	0.00
Tank 8	0	0	0	No. 2 & Jet/Kero	365	8760	0.00
Tank 9	11	2	18	Empty	0	0	0.00
Tank 10	14	2	15	Diesel	365	8760	30.16
Tank 11	14	2	15	No. 2	365	8760	30.16
Tank 12	13	1	15	Jet/Kero	365	8760	21.16
Tank 13	12	2	19	Diesel	365	8760	32.72
Dock Lines							
Gas	5	0	16	Gasoline	365	8760	6.86
No. 2	4	0	8	No. 2	365	8760	6.17
Diesel	4	0	12	Diesel	365	8760	9.00
No. 6	7	0	8	No. 6	0	0	0.00
7 Line	8	1	13	Gasoline	294	7056	7.54
7 Line	8	1	13	No. 2	71	1704	3.71
8 Line	8	1	13	Gasoline	319	7656	8.18
8 Line	8	1	13	No. 2	43	1032	2.25
8 Line	8	1	13	Jet/Kero	3	72	0.16

*Based on AP-42 guidance VOC emissions average about 85 percent of total organic compound (TOC) emissions.

Applicable Average Emission Factors				
	Fittings & Connectors (kg/hr/source)	Pumps (kg/hr/source)	Valves (kg/hr/source)	Others (Compressors & fittings) kg/hr/source
Gas	4.20E-05	6.50E-05	1.30E-05	1.20E-04
Light Liquid	8.00E-06	5.40E-04	4.30E-05	1.30E-04

Fuel Type	2005 VOC Emissions (Tons)
Gasoline	0.02
Jet/Kero	0.02
No. 2/Diesel	0.06
No. 6	0.00
Total VOC Emissions	**0.10**

Equipment leak emissions were calculated using the estimation method from "Protocol for Equipment Leak Emission Estimates" EPA-453/R-93-026 and AP-42, New Equipment Leak Emission Factors, Feb. 1995, from OAQPS TTN bulletin board, using emission factors from Table 2-3, Marketing Terminals Average Emission Factors. The equation has been modified to calculate a VOC emission rate by multiplying the TOC emission rate by 85 percent.

The following equation was used based on the Average Emission Factor Approach, Section 2.3.1:

$$VOC_s = AEF \times WF_{voc} \times N$$

Where:

VOC_s = *VOC Emission Rate* from all equipment in the stream of a given type (kg/hr);

AEF = Applicable *Average Emission Factor* for the equipment type (kg/hr/source)

WF_{voc} = Average liquid mass fraction of VOC in the stream; and

N = Number of pieces of applicable equipment type in the stream.

By Substituting the value of one (1) for WF_{voc}, the resulting equation is:

$$\text{Total VOC Emission Rate} = AEF \times 1 \times N$$

Table 6
Irving Oil Terminals, Inc.
2005 Ballasting Loss Emissions Calculations
(No Ballasting During 2005)

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002001.tn
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Internal Floating Roof Tank
Description:	2005 Operations

Tank Dimensions

Diameter (ft):	162.00
Volume (gallons):	7,350,000.00
Turnovers:	11.87
Self Supp. Roof? (y/n):	N
No. of Columns:	16.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Vapor-mounted
Secondary Seal:	None

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Panel
Deck Seam:	Panel: 5 x 12 Ft
Deck Seam Len. (ft):	5,771.35

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	2
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.	1

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Gasoline (RVP 13)	Jan	35.40	31.29	39.51	45.40	4.2890	N/A	N/A	62.0000			92.00	Option 4: RVP=13, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0072	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5661	N/A	N/A	78.1100	0.0180	0.0035	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.5974	N/A	N/A	84.1600	0.0024	0.0005	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0436	N/A	N/A	106.1700	0.0140	0.0002	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						0.9706	N/A	N/A	86.1700	0.0100	0.0034	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	0.0029	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0192	N/A	N/A	120.2000	0.0050	0.0000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.1200	0.0797	88.15	Option 1: VP40 = 1.92
Toluene						0.1464	N/A	N/A	92.1300	0.0700	0.0035	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						6.2340	N/A	N/A	60.1108	0.6256	0.9052	89.60	
Xylene (-m)						0.0360	N/A	N/A	106.1700	0.0700	0.0009	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 13)	Feb	36.87	32.28	41.45	45.40	4.4203	N/A	N/A	62.0000			92.00	Option 4: RVP=13, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0076	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5926	N/A	N/A	78.1100	0.0180	0.0036	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.6247	N/A	N/A	84.1600	0.0024	0.0005	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0462	N/A	N/A	106.1700	0.0140	0.0002	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0131	N/A	N/A	86.1700	0.0100	0.0034	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	0.0029	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0204	N/A	N/A	120.2000	0.0050	0.0000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.1200	0.0773	88.15	Option 1: VP40 = 1.92
Toluene						0.1541	N/A	N/A	92.1300	0.0700	0.0036	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						6.4354	N/A	N/A	60.1589	0.6256	0.9075	89.60	
Xylene (-m)						0.0382	N/A	N/A	106.1700	0.0700	0.0009	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 13)	Mar	41.56	37.07	46.06	45.40	4.8614	N/A	N/A	62.0000			92.00	Option 4: RVP=13, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0094	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6843	N/A	N/A	78.1100	0.0180	0.0038	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.7189	N/A	N/A	84.1600	0.0024	0.0005	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0554	N/A	N/A	106.1700	0.0140	0.0002	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1593	N/A	N/A	86.1700	0.0100	0.0035	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2402	N/A	N/A	114.2200	0.0400	0.0029	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0248	N/A	N/A	120.2000	0.0050	0.0000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.0106	N/A	N/A	88.1500	0.1200	0.0736	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.1811	N/A	N/A	92.1300	0.0700	0.0039	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						7.0933	N/A	N/A	60.2194	0.6256	0.9104	89.60	
Xylene (-m)						0.0459	N/A	N/A	106.1700	0.0700	0.0010	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Apr	46.44	41.38	51.49	45.40	3.5056	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0116	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7918	N/A	N/A	78.1100	0.0180	0.0056	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.8289	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0666	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3292	N/A	N/A	86.1700	0.0100	0.0052	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.3250	N/A	N/A	114.2200	0.0400	0.0051	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0302	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.2933	N/A	N/A	88.1500	0.1200	0.1078	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.2134	N/A	N/A	92.1300	0.0700	0.0059	92.13	Option 2: A=6.954, B=1344.8, C=219.48

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Unidentified Components						4.9119	N/A	N/A	64.5849	0.6256	0.8676	89.60	
Xylene (-m)						0.0552	N/A	N/A	106.1700	0.0700	0.0015	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	May	51.25	45.58	56.92	45.40	3.8702	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0143	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9115	N/A	N/A	78.1100	0.0180	0.0058	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.9510	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0795	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.5166	N/A	N/A	86.1700	0.0100	0.0054	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4111	N/A	N/A	114.2200	0.0400	0.0058	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0366	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.5899	N/A	N/A	88.1500	0.1200	0.1103	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2499	N/A	N/A	92.1300	0.0700	0.0062	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						5.4044	N/A	N/A	64.4913	0.6256	0.8635	89.60	
Xylene (-m)						0.0660	N/A	N/A	106.1700	0.0700	0.0016	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Jun	55.47	49.47	61.48	45.40	4.2148	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0170	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.0287	N/A	N/A	78.1100	0.0180	0.0060	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.0702	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0925	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6987	N/A	N/A	86.1700	0.0100	0.0055	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4926	N/A	N/A	114.2200	0.0400	0.0064	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0431	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.8941	N/A	N/A	88.1500	0.1200	0.1131	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2863	N/A	N/A	92.1300	0.0700	0.0065	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						5.8648	N/A	N/A	64.3963	0.6256	0.8591	89.60	
Xylene (-m)						0.0769	N/A	N/A	106.1700	0.0700	0.0018	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Jul	58.15	52.19	64.11	45.40	4.4458	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0190	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1092	N/A	N/A	78.1100	0.0180	0.0062	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.1520	N/A	N/A	84.1600	0.0024	0.0009	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.1017	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.8232	N/A	N/A	86.1700	0.0100	0.0056	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.5443	N/A	N/A	114.2200	0.0400	0.0067	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0477	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						3.0868	N/A	N/A	88.1500	0.1200	0.1144	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.3116	N/A	N/A	92.1300	0.0700	0.0067	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						6.1753	N/A	N/A	64.3489	0.6256	0.8570	89.60	
Xylene (-m)						0.0847	N/A	N/A	106.1700	0.0700	0.0018	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Aug	57.30	51.62	62.97	45.40	4.3709	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0183	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.0829	N/A	N/A	78.1100	0.0180	0.0061	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.1253	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0987	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.7826	N/A	N/A	86.1700	0.0100	0.0056	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.5278	N/A	N/A	114.2200	0.0400	0.0066	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0462	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						3.0253	N/A	N/A	88.1500	0.1200	0.1140	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.3033	N/A	N/A	92.1300	0.0700	0.0067	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						6.0745	N/A	N/A	64.3630	0.6256	0.8576	89.60	
Xylene (-m)						0.0821	N/A	N/A	106.1700	0.0700	0.0018	106.17	Option 2: A=7.009, B=1462.266, C=215.11

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Gasoline (RVP 9)	Sep	53.23	47.96	58.50	45.40	4.0290	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0155	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9651	N/A	N/A	78.1100	0.0180	0.0059	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.0055	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0854	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6000	N/A	N/A	86.1700	0.0100	0.0055	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4494	N/A	N/A	114.2200	0.0400	0.0061	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0395	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.7327	N/A	N/A	88.1500	0.1200	0.1118	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2665	N/A	N/A	92.1300	0.0700	0.0064	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						5.6160	N/A	N/A	64.4434	0.6256	0.8613	89.60	
Xylene (-m)						0.0710	N/A	N/A	106.1700	0.0700	0.0017	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Oct	48.01	43.23	52.78	45.40	3.6215	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0125	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8294	N/A	N/A	78.1100	0.0180	0.0057	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.8673	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0706	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3882	N/A	N/A	86.1700	0.0100	0.0053	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.3523	N/A	N/A	114.2200	0.0400	0.0053	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0322	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.3845	N/A	N/A	88.1500	0.1200	0.1085	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.2248	N/A	N/A	92.1300	0.0700	0.0060	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						5.0692	N/A	N/A	64.5563	0.6256	0.8664	89.60	
Xylene (-m)						0.0585	N/A	N/A	106.1700	0.0700	0.0016	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Nov	43.22	39.55	46.89	45.40	3.2779	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0101	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7194	N/A	N/A	78.1100	0.0180	0.0054	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.7548	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0590	N/A	N/A	106.1700	0.0140	0.0003	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.2149	N/A	N/A	86.1700	0.0100	0.0051	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2690	N/A	N/A	114.2200	0.0400	0.0045	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0265	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.1067	N/A	N/A	88.1500	0.1200	0.1059	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.1916	N/A	N/A	92.1300	0.0700	0.0056	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						4.6044	N/A	N/A	64.6543	0.6256	0.8708	89.60	
Xylene (-m)						0.0489	N/A	N/A	106.1700	0.0700	0.0014	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Dec	37.70	34.02	41.39	45.40	2.9154	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0079	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6081	N/A	N/A	78.1100	0.0180	0.0052	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.6407	N/A	N/A	84.1600	0.0024	0.0007	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0478	N/A	N/A	106.1700	0.0140	0.0003	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0380	N/A	N/A	86.1700	0.0100	0.0049	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	0.0040	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0211	N/A	N/A	120.2000	0.0050	0.0000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.1200	0.1085	88.15	Option 1: VP40 = 1.92
Toluene						0.1586	N/A	N/A	92.1300	0.0700	0.0052	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						4.0912	N/A	N/A	64.6402	0.6256	0.8697	89.60	
Xylene (-m)						0.0395	N/A	N/A	106.1700	0.0700	0.0013	106.17	Option 2: A=7.009, B=1462.266, C=215.11

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Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	482.9182	500.5831	561.5883	412.4821	462.4313	511.1699	544.6908	533.7450	484.6997	428.1932	382.0695	334.8567
Seal Factor A (lb-mole/ft-yr):	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Value of Vapor Pressure Function:	0.0861	0.0893	0.1001	0.0681	0.0763	0.0843	0.0899	0.0881	0.0800	0.0707	0.0630	0.0553
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	4.2890	4.4203	4.8614	3.5056	3.8702	4.2148	4.4458	4.3709	4.0290	3.6215	3.2779	2.9154
Tank Diameter (ft):	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000
Vapor Molecular Weight (lb/lb-mole):	62.0000	62.0000	62.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	11.9555	7.8342	8.3208	2.6719	13.9495	5.9149	6.3137	11.0634	6.3071	12.7217	8.9805	15.5544
Number of Columns:	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	9,346,183.000	6,124,386.000	6,504,760.000	2,088,766.000	10,904,999.00	4,624,003.000	4,935,721.000	8,648,806.000	4,930,574.000	9,945,220.000	7,020,520.000	12,159,636.00
	0	0	0	0	00	0	0	0	0	0	0	00
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000
Tank Diameter (ft):	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000
Deck Fitting Losses (lb):	36.4836	37.8181	42.4270	31.1623	34.9358	38.6180	41.1504	40.3235	36.6182	32.3492	28.8647	25.2978
Value of Vapor Pressure Function:	0.0861	0.0893	0.1001	0.0681	0.0763	0.0843	0.0899	0.0881	0.0800	0.0707	0.0630	0.0553
Vapor Molecular Weight (lb/lb-mole):	62.0000	62.0000	62.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000
Deck Seam Losses (lb):	457.7199	474.4631	532.2851	390.9592	438.3021	484.4976	516.2693	505.8947	459.4085	405.8505	362.1335	317.3842
Deck Seam Length (ft):	5,771.3522	5,771.3522	5,771.3522	5,771.3522	5,771.3522	5,771.3522	5,771.3522	5,771.3522	5,771.3522	5,771.3522	5,771.3522	5,771.3522
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800
Tank Diameter (ft):	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000
Vapor Molecular Weight (lb/lb-mole):	62.0000	62.0000	62.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	2	1.60	0.00	0.00	16.6260
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	14.5478
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1	33.00	0.00	0.00	171.4561
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.	1	43.00	0.00	0.00	223.4124

Total Losses (lb):	989.0771	1,020.6986	1,144.6211	837.2755	949.6187	1,040.2004	1,108.4242	1,091.0265	967.0335	879.1147	782.0481	693.0931

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Gasoline (RVP 9)	4,094.34	83.48	309.32	3,880.70	8,367.83
1,2,4-Trimethylbenzene	0.52	2.09	0.04	0.49	3.14
Benzene	23.80	1.50	1.80	22.56	49.66
Cyclohexane	3.31	0.20	0.25	3.14	6.90
Ethylbenzene	1.62	1.17	0.12	1.53	4.44
Hexane (-n)	22.00	0.83	1.66	20.85	45.35
Isooctane	23.61	3.34	1.78	22.37	51.10
Isopropyl benzene	0.27	0.42	0.02	0.25	0.95
Methyl-tert-butyl ether (MTBE)	453.91	10.02	34.29	430.22	928.44
Toluene	25.38	5.84	1.92	24.06	57.21
Unidentified Components	3,533.22	52.22	266.93	3,348.86	7,201.24
Xylene (-m)	6.71	5.84	0.51	6.36	19.42
Gasoline (RVP 13)	1,545.09	28.11	116.73	1,464.47	3,154.40
1,2,4-Trimethylbenzene	0.10	0.70	0.01	0.10	0.91
Benzene	5.61	0.51	0.42	5.31	11.85
Cyclohexane	0.79	0.07	0.06	0.75	1.66
Ethylbenzene	0.34	0.39	0.03	0.33	1.09
Hexane (-n)	5.31	0.28	0.40	5.03	11.03
Isooctane	4.50	1.12	0.34	4.27	10.23
Isopropyl benzene	0.05	0.14	0.00	0.05	0.25
Methyl-tert-butyl ether (MTBE)	118.57	3.37	8.96	112.38	243.28
Toluene	5.70	1.97	0.43	5.40	13.50
Unidentified Components	1,402.69	17.59	105.97	1,329.50	2,855.75
Xylene (-m)	1.42	1.97	0.11	1.35	4.84
Total:	5,639.43	111.59	426.05	5,345.17	11,522.23

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002002
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Internal Floating Roof Tank
Description:	2005 Operations

Tank Dimensions

Diameter (ft):	162.00
Volume (gallons):	7,350,000.00
Turnovers:	9.84
Self Supp. Roof? (y/n):	N
No. of Columns:	16.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	Gray/Light
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Vapor-mounted
Secondary Seal:	None

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Panel
Deck Seam:	Panel: 5 x 12 Ft
Deck Seam Len. (ft):	5,771.35

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	2
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.	1

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	36.89	32.01	41.78	46.51	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031
Benzene						0.5931	N/A	N/A	78.1100	0.0000	0.0111	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0463	N/A	N/A	106.1700	0.0013	0.0274	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0138	N/A	N/A	86.1700	0.0001	0.0236	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1542	N/A	N/A	92.1300	0.0013	0.0957	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0022	N/A	N/A	144.1573	0.9942	0.7869	188.92	
Xylene (-m)						0.0382	N/A	N/A	106.1700	0.0031	0.0553	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Feb	38.79	33.05	44.52	46.51	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031
Benzene						0.6288	N/A	N/A	78.1100	0.0000	0.0117	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0498	N/A	N/A	106.1700	0.0013	0.0295	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0709	N/A	N/A	86.1700	0.0001	0.0250	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1647	N/A	N/A	92.1300	0.0013	0.1022	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0022	N/A	N/A	145.5531	0.9942	0.7720	188.92	
Xylene (-m)						0.0412	N/A	N/A	106.1700	0.0031	0.0596	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Mar	43.97	37.89	50.05	46.51	0.0038	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						0.7358	N/A	N/A	78.1100	0.0000	0.0113	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0607	N/A	N/A	106.1700	0.0013	0.0297	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.2408	N/A	N/A	86.1700	0.0001	0.0239	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1965	N/A	N/A	92.1300	0.0013	0.1006	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0026	N/A	N/A	145.2191	0.9942	0.7745	188.92	
Xylene (-m)						0.0503	N/A	N/A	106.1700	0.0031	0.0600	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Apr	49.24	42.25	56.22	46.51	0.0045	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						0.8598	N/A	N/A	78.1100	0.0000	0.0110	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0739	N/A	N/A	106.1700	0.0013	0.0301	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.4358	N/A	N/A	86.1700	0.0001	0.0230	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2341	N/A	N/A	92.1300	0.0013	0.0998	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0032	N/A	N/A	145.0584	0.9942	0.7752	188.92	
Xylene (-m)						0.0613	N/A	N/A	106.1700	0.0031	0.0609	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	May	54.45	46.50	62.41	46.51	0.0054	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						0.9993	N/A	N/A	78.1100	0.0000	0.0107	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0892	N/A	N/A	106.1700	0.0013	0.0304	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6532	N/A	N/A	86.1700	0.0001	0.0222	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2771	N/A	N/A	92.1300	0.0013	0.0989	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0038	N/A	N/A	144.8923	0.9942	0.7760	188.92	
Xylene (-m)						0.0742	N/A	N/A	106.1700	0.0031	0.0617	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jun	58.92	50.41	67.43	46.51	0.0063	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						1.1333	N/A	N/A	78.1100	0.0000	0.0105	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1045	N/A	N/A	106.1700	0.0013	0.0307	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.8602	N/A	N/A	86.1700	0.0001	0.0215	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3192	N/A	N/A	92.1300	0.0013	0.0982	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0044	N/A	N/A	144.7451	0.9942	0.7768	188.92	
Xylene (-m)						0.0870	N/A	N/A	106.1700	0.0031	0.0624	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jul	61.56	53.13	70.00	46.51	0.0068	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						1.2194	N/A	N/A	78.1100	0.0000	0.0103	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1146	N/A	N/A	106.1700	0.0013	0.0308	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9926	N/A	N/A	86.1700	0.0001	0.0211	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3466	N/A	N/A	92.1300	0.0013	0.0977	92.13	Option 2: A=6.954, B=1344.8, C=219.48

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Unidentified Components						0.0048	N/A	N/A	144.6559	0.9942	0.7773	188.92	
Xylene (-m)						0.0955	N/A	N/A	106.1700	0.0031	0.0627	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Aug	60.40	52.52	68.28	46.51	0.0066	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						1.1809	N/A	N/A	78.1100	0.0000	0.0104	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1101	N/A	N/A	106.1700	0.0013	0.0308	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9334	N/A	N/A	86.1700	0.0001	0.0213	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3343	N/A	N/A	92.1300	0.0013	0.0979	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0046	N/A	N/A	144.6953	0.9942	0.7771	188.92	
Xylene (-m)						0.0917	N/A	N/A	106.1700	0.0031	0.0626	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Sep	55.82	48.81	62.83	46.51	0.0056	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						1.0387	N/A	N/A	78.1100	0.0000	0.0107	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0937	N/A	N/A	106.1700	0.0013	0.0305	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.7143	N/A	N/A	86.1700	0.0001	0.0220	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2894	N/A	N/A	92.1300	0.0013	0.0987	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0040	N/A	N/A	144.8478	0.9942	0.7762	188.92	
Xylene (-m)						0.0779	N/A	N/A	106.1700	0.0031	0.0619	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Oct	49.99	44.01	55.96	46.51	0.0046	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						0.8787	N/A	N/A	78.1100	0.0000	0.0110	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0759	N/A	N/A	106.1700	0.0013	0.0301	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.4654	N/A	N/A	86.1700	0.0001	0.0229	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2399	N/A	N/A	92.1300	0.0013	0.0997	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0033	N/A	N/A	145.0351	0.9942	0.7753	188.92	
Xylene (-m)						0.0630	N/A	N/A	106.1700	0.0031	0.0610	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Nov	44.68	40.27	49.09	46.51	0.0039	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
Benzene						0.7515	N/A	N/A	78.1100	0.0000	0.0113	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0624	N/A	N/A	106.1700	0.0013	0.0297	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.2656	N/A	N/A	86.1700	0.0001	0.0238	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2012	N/A	N/A	92.1300	0.0013	0.1005	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	N/A	N/A	145.1979	0.9942	0.7746	188.92	
Xylene (-m)						0.0517	N/A	N/A	106.1700	0.0031	0.0601	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Dec	39.03	34.72	43.33	46.51	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031
Benzene						0.6334	N/A	N/A	78.1100	0.0000	0.0118	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0503	N/A	N/A	106.1700	0.0013	0.0298	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0783	N/A	N/A	86.1700	0.0001	0.0252	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1660	N/A	N/A	92.1300	0.0013	0.1030	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0022	N/A	N/A	145.7402	0.9942	0.7701	188.92	
Xylene (-m)						0.0416	N/A	N/A	106.1700	0.0031	0.0601	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	0.6205	0.6205	0.7519	0.9030	1.0784	1.2520	1.3660	1.3148	1.1290	0.9264	0.7708	0.6205
Seal Factor A (lb-mole/ft-yr):	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0031	0.0038	0.0045	0.0054	0.0063	0.0068	0.0066	0.0056	0.0046	0.0039	0.0031
Tank Diameter (ft):	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	10.6249	10.7475	1.3630	4.7601	11.2038	8.9968	11.5165	14.0513	10.4925	4.3735	15.0458	14.0952
Number of Columns:	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	6,551,227.000	6,626,819.000	840,410.0000	2,935,015.000	6,908,192.000	5,547,384.000	7,100,955.000	8,663,942.000	6,469,613.000	2,696,672.000	9,277,098.000	8,691,018.000
	0	0		0	0	0	0	0	0	0	0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000
Tank Diameter (ft):	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000
Deck Fitting Losses (lb):	0.0469	0.0469	0.0568	0.0682	0.0815	0.0946	0.1032	0.0993	0.0853	0.0700	0.0582	0.0469
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000	82.0000
Deck Seam Losses (lb):	0.5881	0.5881	0.7126	0.8559	1.0222	1.1866	1.2947	1.2462	1.0701	0.8781	0.7305	0.5881
Deck Seam Length (ft):	5,771.3500	5,771.3500	5,771.3500	5,771.3500	5,771.3500	5,771.3500	5,771.3500	5,771.3500	5,771.3500	5,771.3500	5,771.3500	5,771.3500
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800
Tank Diameter (ft):	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	2	1.60	0.00	0.00	0.0335
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	0.0293
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	1	33.00	0.00	0.00	0.3459
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.	1	43.00	0.00	0.00	0.4507

Total Losses (lb):	11.8803	12.0029	2.8843	6.5872	13.3859	11.5300	14.2804	16.7116	12.7769	6.2481	16.6053	15.3507

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Distillate fuel oil no. 2	11.35	117.27	0.86	10.76	140.24
Benzene	0.12	0.00	0.01	0.12	0.25
Ethylbenzene	0.34	0.15	0.03	0.32	0.84
Hexane (-n)	0.26	0.01	0.02	0.24	0.52
Toluene	1.13	0.16	0.09	1.07	2.43
Unidentified Components	8.81	116.59	0.67	8.35	134.42
Xylene (-m)	0.69	0.36	0.05	0.66	1.77

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002003
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Internal Floating Roof Tank
Description:	2005 Operations

Tank Dimensions

Diameter (ft):	110.00
Volume (gallons):	3,360,000.00
Turnovers:	1.06
Self Supp. Roof? (y/n):	N
No. of Columns:	7.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Vapor-mounted
Secondary Seal:	None

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Panel
Deck Seam:	Panel: 5 x 12 Ft
Deck Seam Len. (ft):	2,660.93

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	2
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	7
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.	1

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Jet kerosene	Jan	35.40	31.29	39.51	45.40	0.0041	N/A	N/A	130.0000			162.00	Option 1: VP40 = .0041
Benzene						0.5661	N/A	N/A	78.1100	0.0000	0.0069	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0436	N/A	N/A	106.1700	0.0013	0.0168	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						0.9706	N/A	N/A	86.1700	0.0001	0.0148	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1464	N/A	N/A	92.1300	0.0013	0.0592	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0034	N/A	N/A	137.5726	0.9942	0.8684	162.55	
Xylene (-m)						0.0360	N/A	N/A	106.1700	0.0031	0.0340	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Feb	36.87	32.28	41.45	45.40	0.0041	N/A	N/A	130.0000			162.00	Option 1: VP40 = .0041
Benzene						0.5926	N/A	N/A	78.1100	0.0000	0.0072	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0462	N/A	N/A	106.1700	0.0013	0.0178	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0131	N/A	N/A	86.1700	0.0001	0.0154	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1541	N/A	N/A	92.1300	0.0013	0.0623	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0034	N/A	N/A	138.0639	0.9942	0.8613	162.55	
Xylene (-m)						0.0382	N/A	N/A	106.1700	0.0031	0.0360	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Mar	41.56	37.07	46.06	45.40	0.0044	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.6843	N/A	N/A	78.1100	0.0000	0.0078	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0554	N/A	N/A	106.1700	0.0013	0.0201	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1593	N/A	N/A	86.1700	0.0001	0.0165	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1811	N/A	N/A	92.1300	0.0013	0.0686	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0035	N/A	N/A	139.1010	0.9942	0.8465	162.55	
Xylene (-m)						0.0459	N/A	N/A	106.1700	0.0031	0.0405	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Apr	46.44	41.38	51.49	45.40	0.0052	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.7918	N/A	N/A	78.1100	0.0000	0.0076	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0666	N/A	N/A	106.1700	0.0013	0.0203	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3292	N/A	N/A	86.1700	0.0001	0.0159	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2134	N/A	N/A	92.1300	0.0013	0.0681	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0042	N/A	N/A	139.0156	0.9942	0.8470	162.55	
Xylene (-m)						0.0552	N/A	N/A	106.1700	0.0031	0.0411	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	May	51.25	45.58	56.92	45.40	0.0061	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.9115	N/A	N/A	78.1100	0.0000	0.0074	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0795	N/A	N/A	106.1700	0.0013	0.0205	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.5166	N/A	N/A	86.1700	0.0001	0.0154	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2499	N/A	N/A	92.1300	0.0013	0.0676	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0049	N/A	N/A	138.9280	0.9942	0.8475	162.55	
Xylene (-m)						0.0660	N/A	N/A	106.1700	0.0031	0.0416	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Jun	55.47	49.47	61.48	45.40	0.0071	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						1.0287	N/A	N/A	78.1100	0.0000	0.0072	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0925	N/A	N/A	106.1700	0.0013	0.0207	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6987	N/A	N/A	86.1700	0.0001	0.0150	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2863	N/A	N/A	92.1300	0.0013	0.0670	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0057	N/A	N/A	138.8489	0.9942	0.8481	162.55	
Xylene (-m)						0.0769	N/A	N/A	106.1700	0.0031	0.0420	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Jul	58.15	52.19	64.11	45.40	0.0077	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						1.1092	N/A	N/A	78.1100	0.0000	0.0071	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1017	N/A	N/A	106.1700	0.0013	0.0208	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.8232	N/A	N/A	86.1700	0.0001	0.0147	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3116	N/A	N/A	92.1300	0.0013	0.0667	92.13	Option 2: A=6.954, B=1344.8, C=219.48

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Unidentified Components						0.0062	N/A	N/A	138.7978	0.9942	0.8484	162.55	
Xylene (-m)						0.0847	N/A	N/A	106.1700	0.0031	0.0422	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Aug	57.30	51.62	62.97	45.40	0.0075	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						1.0829	N/A	N/A	78.1100	0.0000	0.0072	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0987	N/A	N/A	106.1700	0.0013	0.0208	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.7826	N/A	N/A	86.1700	0.0001	0.0148	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3033	N/A	N/A	92.1300	0.0013	0.0668	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0060	N/A	N/A	138.8142	0.9942	0.8483	162.55	
Xylene (-m)						0.0821	N/A	N/A	106.1700	0.0031	0.0422	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Sep	53.23	47.96	58.50	45.40	0.0066	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.9651	N/A	N/A	78.1100	0.0000	0.0073	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0854	N/A	N/A	106.1700	0.0013	0.0206	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6000	N/A	N/A	86.1700	0.0001	0.0152	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2665	N/A	N/A	92.1300	0.0013	0.0673	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0053	N/A	N/A	138.8912	0.9942	0.8478	162.55	
Xylene (-m)						0.0710	N/A	N/A	106.1700	0.0031	0.0418	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Oct	48.01	43.23	52.78	45.40	0.0055	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.8294	N/A	N/A	78.1100	0.0000	0.0075	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0706	N/A	N/A	106.1700	0.0013	0.0204	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3882	N/A	N/A	86.1700	0.0001	0.0158	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2248	N/A	N/A	92.1300	0.0013	0.0679	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0044	N/A	N/A	138.9873	0.9942	0.8472	162.55	
Xylene (-m)						0.0585	N/A	N/A	106.1700	0.0031	0.0412	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Nov	43.22	39.55	46.89	45.40	0.0046	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.7194	N/A	N/A	78.1100	0.0000	0.0077	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0590	N/A	N/A	106.1700	0.0013	0.0201	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.2149	N/A	N/A	86.1700	0.0001	0.0163	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1916	N/A	N/A	92.1300	0.0013	0.0685	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0037	N/A	N/A	139.0724	0.9942	0.8467	162.55	
Xylene (-m)						0.0489	N/A	N/A	106.1700	0.0031	0.0407	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Dec	37.70	34.02	41.39	45.40	0.0041	N/A	N/A	130.0000			162.00	Option 1: VP40 = .0041
Benzene						0.6081	N/A	N/A	78.1100	0.0000	0.0074	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0478	N/A	N/A	106.1700	0.0013	0.0184	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0380	N/A	N/A	86.1700	0.0001	0.0158	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1586	N/A	N/A	92.1300	0.0013	0.0641	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0033	N/A	N/A	138.3591	0.9942	0.8571	162.55	
Xylene (-m)						0.0395	N/A	N/A	106.1700	0.0031	0.0372	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	0.5572	0.5572	0.5945	0.7058	0.8335	0.9620	1.0523	1.0227	0.8918	0.7455	0.6304	0.5572
Seal Factor A (lb-mole/ft-yr):	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0041	0.0041	0.0044	0.0052	0.0061	0.0071	0.0077	0.0075	0.0066	0.0055	0.0046	0.0041
Tank Diameter (ft):	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	0.0000	0.0000	0.0000	0.0000	1.9187	0.0000	0.0000	0.0000	0.0000	0.0000	2.3632	3.8346
Number of Columns:	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	0.0000	0.0000	0.0000	0.0000	841,704.0000	0.0000	0.0000	0.0000	0.0000	0.0000	1,036,683.000	1,682,150.000
											0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000
Tank Diameter (ft):	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000
Deck Fitting Losses (lb):	0.2117	0.2117	0.2259	0.2681	0.3167	0.3655	0.3998	0.3885	0.3388	0.2832	0.2395	0.2117
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	280.0000	280.0000	280.0000	280.0000	280.0000	280.0000	280.0000	280.0000	280.0000	280.0000	280.0000	280.0000
Deck Seam Losses (lb):	0.3586	0.3586	0.3826	0.4542	0.5364	0.6192	0.6772	0.6582	0.5739	0.4798	0.4057	0.3586
Deck Seam Length (ft):	2,660.9300	2,660.9300	2,660.9300	2,660.9300	2,660.9300	2,660.9300	2,660.9300	2,660.9300	2,660.9300	2,660.9300	2,660.9300	2,660.9300
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800	0.2800
Tank Diameter (ft):	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	2	1.60	0.00	0.00	0.0396
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	0.0347
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.	7	33.00	0.00	0.00	2.8601
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.	1	43.00	0.00	0.00	0.5324

Total Losses (lb):	1.1276	1.1276	1.2029	1.4282	3.6053	1.9467	2.1293	2.0694	1.8046	1.5085	3.6389	4.9621

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Jet kerosene	9.11	8.12	3.46	5.86	26.55
Benzene	0.07	0.00	0.03	0.04	0.14
Ethylbenzene	0.18	0.01	0.07	0.12	0.38
Hexane (-n)	0.14	0.00	0.05	0.09	0.28
Toluene	0.61	0.01	0.23	0.39	1.24
Unidentified Components	7.75	8.07	2.94	4.99	23.74
Xylene (-m)	0.37	0.03	0.14	0.24	0.77

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002004
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Vertical Fixed Roof Tank
Description:	2005 Operations-No emissions are associated with this tank because it is no longer operational.

Tank Dimensions

Shell Height (ft):	48.00
Diameter (ft):	162.00
Liquid Height (ft):	48.00
Avg. Liquid Height (ft):	24.00
Volume (gallons):	7,401,812.00
Turnovers:	0.00
Net Throughput (gal/yr):	0.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	Gray/Medium
Shell Condition:	Good
Roof Color/Shade:	Gray/Medium
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	5.06
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	0.00
Pressure Settings (psig):	0.00

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Residual oil no. 6	Jan	39.52	33.27	45.76	48.46	0.0000	0.0000	0.0000	190.0000			387.00	Option 1: VP40 = .00002
Benzene						0.6430	0.5296	0.7762	78.1100	0.0000	0.0065	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0512	0.0401	0.0650	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.1689	0.1358	0.2087	92.1300	0.0000	0.0053	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	193.2972	1.0000	0.9859	387.00	
Xylene (-o)						0.0328	0.0255	0.0419	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Feb	42.16	34.40	49.91	48.46	0.0000	0.0000	0.0000	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						0.6968	0.5487	0.8769	78.1100	0.0000	0.0067	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0567	0.0420	0.0757	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.1848	0.1413	0.2393	92.1300	0.0000	0.0056	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	193.4220	1.0000	0.9853	387.00	
Xylene (-o)						0.0364	0.0267	0.0490	106.1700	0.0000	0.0018	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Mar	48.20	39.34	57.05	48.46	0.0000	0.0000	0.0000	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						0.8340	0.6395	1.0756	78.1100	0.0000	0.0063	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0711	0.0509	0.0979	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.2262	0.1679	0.3010	92.1300	0.0000	0.0053	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	193.2326	1.0000	0.9861	387.00	
Xylene (-o)						0.0459	0.0326	0.0639	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Apr	54.16	43.78	64.54	48.46	0.0000	0.0000	0.0001	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						0.9911	0.7317	1.3229	78.1100	0.0000	0.0059	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0883	0.0603	0.1269	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.2746	0.1953	0.3797	92.1300	0.0000	0.0051	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	193.0576	1.0000	0.9868	387.00	
Xylene (-o)						0.0575	0.0388	0.0835	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	May	60.08	48.11	72.06	48.46	0.0000	0.0000	0.0001	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						1.1705	0.8318	1.6167	78.1100	0.0000	0.0055	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1088	0.0709	0.1632	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.3310	0.2255	0.4756	92.1300	0.0000	0.0048	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	192.8951	1.0000	0.9874	387.00	
Xylene (-o)						0.0713	0.0458	0.1082	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Jun	64.97	52.07	77.87	48.46	0.0001	0.0000	0.0001	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						1.3383	0.9333	1.8792	78.1100	0.0000	0.0052	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1288	0.0819	0.1970	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.3847	0.2567	0.5631	92.1300	0.0000	0.0047	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0001	0.0001	0.0001	192.7688	1.0000	0.9879	387.00	
Xylene (-o)						0.0848	0.0532	0.1314	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Jul	67.56	54.78	80.34	48.46	0.0001	0.0000	0.0001	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						1.4350	1.0086	2.0008	78.1100	0.0000	0.0051	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1405	0.0903	0.2131	106.1700	0.0000	0.0005	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.4160	0.2800	0.6042	92.1300	0.0000	0.0046	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0001	0.0001	0.0001	192.7046	1.0000	0.9882	387.00	
Xylene (-o)						0.0928	0.0588	0.1425	106.1700	0.0000	0.0016	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Aug	65.85	54.11	77.60	48.46	0.0001	0.0000	0.0001	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						1.3707	0.9897	1.8660	78.1100	0.0000	0.0052	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1327	0.0882	0.1953	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.3952	0.2741	0.5587	92.1300	0.0000	0.0046	92.13	Option 2: A=6.954, B=1344.8, C=219.48

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Unidentified Components						0.0001	0.0001	0.0001	192.7467	1.0000	0.9880	387.00	
Xylene (-o)						0.0874	0.0574	0.1302	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Sep	60.36	50.29	70.42	48.46	0.0000	0.0000	0.0001	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						1.1795	0.8866	1.5486	78.1100	0.0000	0.0055	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1099	0.0768	0.1546	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.3338	0.2423	0.4532	92.1300	0.0000	0.0048	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	192.8878	1.0000	0.9874	387.00	
Xylene (-o)						0.0720	0.0497	0.1024	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Oct	53.46	45.37	61.54	48.46	0.0000	0.0000	0.0000	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						0.9713	0.7673	1.2187	78.1100	0.0000	0.0059	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0861	0.0640	0.1145	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.2684	0.2060	0.3463	92.1300	0.0000	0.0051	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	193.0777	1.0000	0.9867	387.00	
Xylene (-o)						0.0560	0.0412	0.0751	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Nov	47.24	41.53	52.95	48.46	0.0000	0.0000	0.0000	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						0.8108	0.6836	0.9572	78.1100	0.0000	0.0064	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0686	0.0554	0.0845	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.2191	0.1809	0.2640	92.1300	0.0000	0.0053	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	193.2619	1.0000	0.9860	387.00	
Xylene (-o)						0.0443	0.0355	0.0549	106.1700	0.0000	0.0017	106.17	Option 2: A=6.998, B=1474.679, C=213.69
Residual oil no. 6	Dec	41.35	35.95	46.74	48.46	0.0000	0.0000	0.0000	190.0000			387.00	Option 5: A=10.104, B=10475
Benzene						0.6799	0.5760	0.7990	78.1100	0.0000	0.0068	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0550	0.0446	0.0674	106.1700	0.0000	0.0006	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Toluene						0.1798	0.1492	0.2156	92.1300	0.0000	0.0056	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0000	0.0000	0.0000	193.4485	1.0000	0.9852	387.00	
Xylene (-o)						0.0352	0.0284	0.0435	106.1700	0.0000	0.0018	106.17	Option 2: A=6.998, B=1474.679, C=213.69

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	0.5826	0.6799	1.0757	1.5145	2.2258	2.7479	3.0725	2.6634	1.8280	1.1885	0.6478	0.5077
Vapor Space Volume (cu ft):	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771
Vapor Density (lb/cu ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Space Expansion Factor:	0.0500	0.0618	0.0698	0.0808	0.0922	0.0984	0.0970	0.0894	0.0774	0.0630	0.0451	0.0431
Vented Vapor Saturation Factor:	1.0000	1.0000	1.0000	1.0000	0.9999	0.9999	0.9999	0.9999	0.9999	1.0000	1.0000	1.0000
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771	529,470.4771
Tank Diameter (ft):	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000
Vapor Space Outage (ft):	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875
Tank Shell Height (ft):	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000
Average Liquid Height (ft):	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000
Roof Outage (ft):	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875
Roof Outage (Cone Roof)												
Roof Outage (ft):	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875	1.6875
Roof Height (ft):	5.0625	5.0625	5.0625	5.0625	5.0625	5.0625	5.0625	5.0625	5.0625	5.0625	5.0625	5.0625
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	81.0000	81.0000	81.0000	81.0000	81.0000	81.0000	81.0000	81.0000	81.0000	81.0000	81.0000	81.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (lb/lb-mole):	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0001	0.0001	0.0001	0.0000	0.0000	0.0000	0.0000
Daily Avg. Liquid Surface Temp. (deg. R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Average Ambient Temp. (deg. F):	20.8500	23.3000	32.9500	43.2000	53.3000	62.4000	68.5500	67.2500	59.1000	48.5000	38.7000	26.4500
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292
Tank Paint Solar Absorptance (Shell):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Tank Paint Solar Absorptance (Roof):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Daily Total Solar Insulation Factor (Btu/sqft day):	597.1021	888.0387	1,221.4895	1,492.4381	1,767.1939	1,931.5398	1,909.9654	1,698.9809	1,343.3212	927.0629	571.7205	478.7604
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0500	0.0618	0.0698	0.0808	0.0922	0.0984	0.0970	0.0894	0.0774	0.0630	0.0451	0.0431
Daily Vapor Temperature Range (deg. R):	24.9768	31.0203	35.4252	41.5200	47.9034	51.6085	51.1257	46.9646	40.2648	32.3393	22.8376	21.5716
Daily Vapor Pressure Range (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0001	0.0001	0.0000	0.0000	0.0000	0.0000	0.0000
Breather Vent Press. Setting Range(psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0001	0.0001	0.0001	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0000	0.0000	0.0000
Daily Avg. Liquid Surface Temp. (deg R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Min. Liquid Surface Temp. (deg R):	492.9446	494.0746	499.0107	503.4525	507.7767	511.7372	514.4480	513.7829	509.9612	505.0425	501.1970	495.6241
Daily Max. Liquid Surface Temp. (deg R):	505.4330	509.5847	516.7233	524.2125	531.7283	537.5415	540.0109	537.2652	530.0937	521.2121	512.6158	506.4099
Daily Ambient Temp. Range (deg. R):	18.9000	19.6000	16.9000	18.2000	19.8000	20.6000	20.5000	20.3000	20.4000	20.4000	16.6000	17.3000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	1.0000	1.0000	1.0000	1.0000	0.9999	0.9999	0.9999	0.9999	0.9999	1.0000	1.0000	1.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0001	0.0001	0.0001	0.0000	0.0000	0.0000	0.0000
Vapor Space Outage (ft):	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875	25.6875

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (lb/lb-mole):	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000	190.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0001	0.0001	0.0001	0.0000	0.0000	0.0000	0.0000
Net Throughput (gal/mo.):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Annual Turnovers:	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000	7,401,812.000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000	48.0000
Tank Diameter (ft):	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000	162.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	0.5826	0.6799	1.0757	1.5145	2.2258	2.7479	3.0725	2.6634	1.8280	1.1885	0.6478	0.5077

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Residual oil no. 6	0.00	18.73	18.73
Benzene	0.00	0.10	0.10
Ethylbenzene	0.00	0.01	0.01
Toluene	0.00	0.09	0.09
Unidentified Components	0.00	18.50	18.50
Xylene (-o)	0.00	0.03	0.03

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002005.tn
City:	Searsport
State:	Maine
Company:	Irving Oil Corp.
Type of Tank:	Internal Floating Roof Tank
Description:	2005 Operations

Tank Dimensions

Diameter (ft):	110.00
Volume (gallons):	3,360,000.00
Turnovers:	1.01
Self Supp. Roof? (y/n):	N
No. of Columns:	7.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Liquid-mounted
Secondary Seal:	None

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Sheet
Deck Seam:	Sheet: 5 Ft Wide
Deck Seam Len. (ft):	1,900.66

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Unbolted Cover, Gasketed	2
Automatic Gauge Float Well/Unbolted Cover, Ungasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Ungask.	7
Ladder Well (36-in. Diam.)/Sliding Cover, Ungasketed	1
Roof Leg or Hanger Well/Adjustable	37
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1
Stub Drain (1-in. Diameter)/	97

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask. 1

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Gasoline (RVP 13)	Jan	35.40	31.29	39.51	45.40	4.2890	N/A	N/A	62.0000			92.00	Option 4: RVP=13, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0072	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5661	N/A	N/A	78.1100	0.0180	0.0035	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.5974	N/A	N/A	84.1600	0.0024	0.0005	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0436	N/A	N/A	106.1700	0.0140	0.0002	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						0.9706	N/A	N/A	86.1700	0.0100	0.0034	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	0.0029	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0192	N/A	N/A	120.2000	0.0050	0.0000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.1200	0.0797	88.15	Option 1: VP40 = 1.92
Toluene						0.1464	N/A	N/A	92.1300	0.0700	0.0035	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						6.2340	N/A	N/A	60.1108	0.6256	0.9052	89.60	
Xylene (-m)						0.0360	N/A	N/A	106.1700	0.0700	0.0009	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 13)	Feb	36.87	32.28	41.45	45.40	4.4203	N/A	N/A	62.0000			92.00	Option 4: RVP=13, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0076	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5926	N/A	N/A	78.1100	0.0180	0.0036	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.6247	N/A	N/A	84.1600	0.0024	0.0005	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0462	N/A	N/A	106.1700	0.0140	0.0002	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0131	N/A	N/A	86.1700	0.0100	0.0034	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	0.0029	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0204	N/A	N/A	120.2000	0.0050	0.0000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.1200	0.0773	88.15	Option 1: VP40 = 1.92
Toluene						0.1541	N/A	N/A	92.1300	0.0700	0.0036	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						6.4354	N/A	N/A	60.1589	0.6256	0.9075	89.60	
Xylene (-m)						0.0382	N/A	N/A	106.1700	0.0700	0.0009	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 13)	Mar	41.56	37.07	46.06	45.40	4.8614	N/A	N/A	62.0000			92.00	Option 4: RVP=13, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0094	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6843	N/A	N/A	78.1100	0.0180	0.0038	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.7189	N/A	N/A	84.1600	0.0024	0.0005	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0554	N/A	N/A	106.1700	0.0140	0.0002	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1593	N/A	N/A	86.1700	0.0100	0.0035	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2402	N/A	N/A	114.2200	0.0400	0.0029	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0248	N/A	N/A	120.2000	0.0050	0.0000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.0106	N/A	N/A	88.1500	0.1200	0.0736	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.1811	N/A	N/A	92.1300	0.0700	0.0039	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						7.0933	N/A	N/A	60.2194	0.6256	0.9104	89.60	
Xylene (-m)						0.0459	N/A	N/A	106.1700	0.0700	0.0010	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Apr	46.44	41.38	51.49	45.40	3.5056	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0116	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7918	N/A	N/A	78.1100	0.0180	0.0056	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.8289	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0666	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3292	N/A	N/A	86.1700	0.0100	0.0052	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.3250	N/A	N/A	114.2200	0.0400	0.0051	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0302	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.2933	N/A	N/A	88.1500	0.0880	0.0790	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.2134	N/A	N/A	92.1300	0.0700	0.0059	92.13	Option 2: A=6.954, B=1344.8, C=219.48

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Unidentified Components						4.7825	N/A	N/A	65.1433	0.6576	0.8964	89.52	
Xylene (-m)						0.0552	N/A	N/A	106.1700	0.0700	0.0015	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	May	51.25	45.58	56.92	45.40	3.8702	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0143	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9115	N/A	N/A	78.1100	0.0180	0.0058	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.9510	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0795	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.5166	N/A	N/A	86.1700	0.0100	0.0054	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4111	N/A	N/A	114.2200	0.0400	0.0058	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0366	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.5899	N/A	N/A	88.1500	0.0880	0.0809	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2499	N/A	N/A	92.1300	0.0700	0.0062	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						5.2653	N/A	N/A	65.0665	0.6576	0.8929	89.52	
Xylene (-m)						0.0660	N/A	N/A	106.1700	0.0700	0.0016	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Jun	55.47	49.47	61.48	45.40	4.2148	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0170	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.0287	N/A	N/A	78.1100	0.0180	0.0060	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.0702	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0925	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6987	N/A	N/A	86.1700	0.0100	0.0055	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4926	N/A	N/A	114.2200	0.0400	0.0064	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0431	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.8941	N/A	N/A	88.1500	0.0880	0.0830	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2863	N/A	N/A	92.1300	0.0700	0.0065	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						5.7180	N/A	N/A	64.9904	0.6576	0.8893	89.52	
Xylene (-m)						0.0769	N/A	N/A	106.1700	0.0700	0.0018	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Jul	58.15	52.19	64.11	45.40	4.4458	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0190	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1092	N/A	N/A	78.1100	0.0180	0.0062	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.1520	N/A	N/A	84.1600	0.0024	0.0009	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.1017	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.8232	N/A	N/A	86.1700	0.0100	0.0056	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.5443	N/A	N/A	114.2200	0.0400	0.0067	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0477	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						3.0868	N/A	N/A	88.1500	0.0880	0.0839	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.3116	N/A	N/A	92.1300	0.0700	0.0067	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						6.0227	N/A	N/A	64.9518	0.6576	0.8875	89.52	
Xylene (-m)						0.0847	N/A	N/A	106.1700	0.0700	0.0018	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Aug	57.30	51.62	62.97	45.40	4.3709	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0183	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.0829	N/A	N/A	78.1100	0.0180	0.0061	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.1253	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0987	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.7826	N/A	N/A	86.1700	0.0100	0.0056	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.5278	N/A	N/A	114.2200	0.0400	0.0066	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0462	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						3.0253	N/A	N/A	88.1500	0.0880	0.0836	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.3033	N/A	N/A	92.1300	0.0700	0.0067	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						5.9238	N/A	N/A	64.9634	0.6576	0.8880	89.52	
Xylene (-m)						0.0821	N/A	N/A	106.1700	0.0700	0.0018	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Gasoline (RVP 9)	Sep	53.23	47.96	58.50	45.40	4.0290	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0155	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9651	N/A	N/A	78.1100	0.0180	0.0059	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.0055	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0854	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6000	N/A	N/A	86.1700	0.0100	0.0055	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4494	N/A	N/A	114.2200	0.0400	0.0061	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0395	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.7327	N/A	N/A	88.1500	0.0880	0.0820	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2665	N/A	N/A	92.1300	0.0700	0.0064	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						5.4735	N/A	N/A	65.0283	0.6576	0.8911	89.52	
Xylene (-m)						0.0710	N/A	N/A	106.1700	0.0700	0.0017	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Oct	48.01	43.23	52.78	45.40	3.6215	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0125	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8294	N/A	N/A	78.1100	0.0180	0.0057	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.8673	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0706	N/A	N/A	106.1700	0.0140	0.0004	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3882	N/A	N/A	86.1700	0.0100	0.0053	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.3523	N/A	N/A	114.2200	0.0400	0.0053	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0322	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.3845	N/A	N/A	88.1500	0.0880	0.0796	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.2248	N/A	N/A	92.1300	0.0700	0.0060	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						4.9365	N/A	N/A	65.1196	0.6576	0.8953	89.52	
Xylene (-m)						0.0585	N/A	N/A	106.1700	0.0700	0.0016	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Nov	43.22	39.55	46.89	45.40	3.2779	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0101	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7194	N/A	N/A	78.1100	0.0180	0.0054	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.7548	N/A	N/A	84.1600	0.0024	0.0008	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0590	N/A	N/A	106.1700	0.0140	0.0003	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.2149	N/A	N/A	86.1700	0.0100	0.0051	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2690	N/A	N/A	114.2200	0.0400	0.0045	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0265	N/A	N/A	120.2000	0.0050	0.0001	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.1067	N/A	N/A	88.1500	0.0880	0.0777	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.1916	N/A	N/A	92.1300	0.0700	0.0056	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						4.4809	N/A	N/A	65.2002	0.6576	0.8990	89.52	
Xylene (-m)						0.0489	N/A	N/A	106.1700	0.0700	0.0014	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Gasoline (RVP 9)	Dec	37.70	34.02	41.39	45.40	2.9154	N/A	N/A	67.0000			92.00	Option 4: RVP=9, ASTM Slope=3
1,2,4-Trimethylbenzene						0.0079	N/A	N/A	120.1900	0.0250	0.0001	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6081	N/A	N/A	78.1100	0.0180	0.0052	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.6407	N/A	N/A	84.1600	0.0024	0.0007	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0478	N/A	N/A	106.1700	0.0140	0.0003	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0380	N/A	N/A	86.1700	0.0100	0.0049	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	0.0040	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0211	N/A	N/A	120.2000	0.0050	0.0000	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.0880	0.0796	88.15	Option 1: VP40 = 1.92
Toluene						0.1586	N/A	N/A	92.1300	0.0700	0.0052	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						3.9839	N/A	N/A	65.2001	0.6576	0.8986	89.52	
Xylene (-m)						0.0395	N/A	N/A	106.1700	0.0700	0.0013	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	78.3062	81.1707	91.0628	66.8849	74.9843	82.8873	88.3228	86.5479	78.5951	69.4325	61.9534	54.2978
Seal Factor A (lb-mole/ft-yr):	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000
Value of Vapor Pressure Function:	0.0861	0.0893	0.1001	0.0681	0.0763	0.0843	0.0899	0.0881	0.0800	0.0707	0.0630	0.0553
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	4.2890	4.4203	4.8614	3.5056	3.8702	4.2148	4.4458	4.3709	4.0290	3.6215	3.2779	2.9154
Tank Diameter (ft):	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000
Vapor Molecular Weight (lb/lb-mole):	62.0000	62.0000	62.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	0.0000	0.0000	1.2542	0.0000	1.9170	0.0000	1.6620	0.0000	0.9873	0.0000	0.3699	0.0000
Number of Columns:	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	0.0000	0.0000	687,757.0000	0.0000	1,051,186.000 0	0.0000	911,356.0000	0.0000	541,392.0000	0.0000	202,826.0000	0.0000
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000	5.6000
Tank Diameter (ft):	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000
Deck Fitting Losses (lb):	403.9445	418.7207	469.7494	345.0272	386.8080	427.5762	455.6153	446.4594	405.4347	358.1690	319.5881	280.0962
Value of Vapor Pressure Function:	0.0861	0.0893	0.1001	0.0681	0.0763	0.0843	0.0899	0.0881	0.0800	0.0707	0.0630	0.0553
Vapor Molecular Weight (lb/lb-mole):	62.0000	62.0000	62.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	907.9000	907.9000	907.9000	907.9000	907.9000	907.9000	907.9000	907.9000	907.9000	907.9000	907.9000	907.9000
Deck Seam Losses (lb):	150.7394	156.2533	175.2957	128.7533	144.3446	159.5580	170.0212	166.6046	151.2955	133.6574	119.2602	104.5231
Deck Seam Length (ft):	1,900.6600	1,900.6600	1,900.6600	1,900.6600	1,900.6600	1,900.6600	1,900.6600	1,900.6600	1,900.6600	1,900.6600	1,900.6600	1,900.6600
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Tank Diameter (ft):	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000
Vapor Molecular Weight (lb/lb-mole):	62.0000	62.0000	62.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000	67.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Unbolted Cover, Gasketed	2	31.00	5.20	1.30	322.1296
Automatic Gauge Float Well/Unbolted Cover, Ungasketed	1	14.00	5.40	1.10	72.7389
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Ungask.	7	47.00	0.00	0.00	1,709.3649
Ladder Well (36-in. Diam.)/Sliding Cover, Ungasketed	1	76.00	0.00	0.00	394.8685
Roof Leg or Hanger Well/Adjustable	37	7.90	0.00	0.00	1,518.6850
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1	12.00	0.00	0.00	62.3477
Stub Drain (1-in. Diameter)/	97	1.20	0.00	0.00	604.7723
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	32.2130

Total Losses (lb):	632.9902	656.1447	737.3621	540.6654	608.0538	670.0215	715.6213	699.6120	636.3126	561.2589	501.1716	438.9170

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Gasoline (RVP 13)	250.54	1.25	1,292.41	482.29	2,026.50
1,2,4-Trimethylbenzene	0.02	0.03	0.09	0.03	0.17
Benzene	0.91	0.02	4.69	1.75	7.37
Cyclohexane	0.13	0.00	0.66	0.25	1.03
Ethylbenzene	0.06	0.02	0.29	0.11	0.47
Hexane (-n)	0.86	0.01	4.44	1.66	6.97
Isooctane	0.73	0.05	3.77	1.41	5.95
Isopropyl benzene	0.01	0.01	0.05	0.02	0.08
Methyl-tert-butyl ether (MTBE)	19.23	0.15	99.18	37.01	155.57
Toluene	0.92	0.09	4.77	1.78	7.56
Unidentified Components	227.45	0.78	1,173.31	437.84	1,839.38
Xylene (-m)	0.23	0.09	1.19	0.44	1.95
Gasoline (RVP 9)	663.91	4.94	3,424.77	1,278.02	5,371.63
1,2,4-Trimethylbenzene	0.08	0.12	0.43	0.16	0.80
Benzene	3.86	0.09	19.91	7.43	31.28
Cyclohexane	0.54	0.01	2.77	1.03	4.35
Ethylbenzene	0.26	0.07	1.35	0.50	2.19
Hexane (-n)	3.57	0.05	18.40	6.87	28.89
Isooctane	3.83	0.20	19.75	7.37	31.14
Isopropyl benzene	0.04	0.02	0.22	0.08	0.37
Methyl-tert-butyl ether (MTBE)	53.97	0.43	278.43	103.90	436.74
Toluene	4.12	0.35	21.23	7.92	33.62
Unidentified Components	592.55	3.25	3,056.67	1,140.65	4,793.11
Xylene (-m)	1.09	0.35	5.61	2.09	9.14
Total:	914.45	6.19	4,717.19	1,760.31	7,398.13

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002006.tn
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Internal Floating Roof Tank
Description:	2005 Operations

Tank Dimensions

Diameter (ft):	137.00
Volume (gallons):	5,250,000.00
Turnovers:	10.08
Self Supp. Roof? (y/n):	N
No. of Columns:	9.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Liquid-mounted
Secondary Seal:	None

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Bolted
Construction:	Sheet
Deck Seam:	Sheet: 5 Ft Wide
Deck Seam Len. (ft):	2,948.23

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Unbolted Cover, Ungasketed	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Ungask.	1
Ladder Well (36-in. Diam.)/Sliding Cover, Ungasketed	1
Roof Leg or Hanger Well/Adjustable	1
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1
Stub Drain (1-in. Diameter)/	1

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Automatic Gauge Float Well/Unbolted Cover, Ungasketed 1

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	35.40	31.29	39.51	45.40	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031
1,2,4-Trimethylbenzene						0.0072	N/A	N/A	120.1900	0.0100	0.0334	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5661	N/A	N/A	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0436	N/A	N/A	106.1700	0.0001	0.0026	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						0.9706	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1464	N/A	N/A	92.1300	0.0003	0.0219	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	N/A	N/A	133.7346	0.9866	0.8908	189.60	
Xylene (-m)						0.0360	N/A	N/A	106.1700	0.0029	0.0488	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Feb	36.87	32.28	41.45	45.40	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031
1,2,4-Trimethylbenzene						0.0076	N/A	N/A	120.1900	0.0100	0.0357	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5926	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0462	N/A	N/A	106.1700	0.0001	0.0028	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0131	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1541	N/A	N/A	92.1300	0.0003	0.0230	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	N/A	N/A	133.9659	0.9866	0.8842	189.60	
Xylene (-m)						0.0382	N/A	N/A	106.1700	0.0029	0.0517	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Mar	41.56	37.07	46.06	45.40	0.0035	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0094	N/A	N/A	120.1900	0.0100	0.0395	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6843	N/A	N/A	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0554	N/A	N/A	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1593	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1811	N/A	N/A	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0030	N/A	N/A	134.3258	0.9866	0.8747	189.60	
Xylene (-m)						0.0459	N/A	N/A	106.1700	0.0029	0.0557	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Apr	46.44	41.38	51.49	45.40	0.0041	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0116	N/A	N/A	120.1900	0.0100	0.0411	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7918	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0666	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3292	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2134	N/A	N/A	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0035	N/A	N/A	134.3696	0.9866	0.8725	189.60	
Xylene (-m)						0.0552	N/A	N/A	106.1700	0.0029	0.0565	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	May	51.25	45.58	56.92	45.40	0.0048	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0143	N/A	N/A	120.1900	0.0100	0.0427	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9115	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0795	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.5166	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2499	N/A	N/A	92.1300	0.0003	0.0239	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0042	N/A	N/A	134.4098	0.9866	0.8703	189.60	
Xylene (-m)						0.0660	N/A	N/A	106.1700	0.0029	0.0573	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jun	55.47	49.47	61.48	45.40	0.0056	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0170	N/A	N/A	120.1900	0.0100	0.0441	120.19	Option 2: A=7.04383, B=1573.267, C=208.56

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Liquid Contents of Storage Tank - (Continued)

Benzene						1.0287	N/A	N/A	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0925	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6987	N/A	N/A	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2863	N/A	N/A	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0048	N/A	N/A	134.4425	0.9866	0.8686	189.60	
Xylene (-m)						0.0769	N/A	N/A	106.1700	0.0029	0.0579	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jul	58.15	52.19	64.11	45.40	0.0061	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0190	N/A	N/A	120.1900	0.0100	0.0450	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1092	N/A	N/A	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1017	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.8232	N/A	N/A	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3116	N/A	N/A	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0052	N/A	N/A	134.4620	0.9866	0.8675	189.60	
Xylene (-m)						0.0847	N/A	N/A	106.1700	0.0029	0.0582	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Aug	57.30	51.62	62.97	45.40	0.0059	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0183	N/A	N/A	120.1900	0.0100	0.0447	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.0829	N/A	N/A	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0987	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.7826	N/A	N/A	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3033	N/A	N/A	92.1300	0.0003	0.0237	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0051	N/A	N/A	134.4559	0.9866	0.8678	189.60	
Xylene (-m)						0.0821	N/A	N/A	106.1700	0.0029	0.0581	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Sep	53.23	47.96	58.50	45.40	0.0052	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0155	N/A	N/A	120.1900	0.0100	0.0434	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9651	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0854	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6000	N/A	N/A	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2665	N/A	N/A	92.1300	0.0003	0.0239	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0044	N/A	N/A	134.4254	0.9866	0.8695	189.60	
Xylene (-m)						0.0710	N/A	N/A	106.1700	0.0029	0.0576	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Oct	48.01	43.23	52.78	45.40	0.0043	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0125	N/A	N/A	120.1900	0.0100	0.0416	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8294	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0706	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3882	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2248	N/A	N/A	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0037	N/A	N/A	134.3831	0.9866	0.8718	189.60	
Xylene (-m)						0.0585	N/A	N/A	106.1700	0.0029	0.0568	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Nov	43.22	39.55	46.89	45.40	0.0037	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0101	N/A	N/A	120.1900	0.0100	0.0400	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7194	N/A	N/A	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0590	N/A	N/A	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.2149	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1916	N/A	N/A	92.1300	0.0003	0.0242	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0032	N/A	N/A	134.3410	0.9866	0.8739	189.60	
Xylene (-m)						0.0489	N/A	N/A	106.1700	0.0029	0.0560	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Dec	37.70	34.02	41.39	45.40	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

1,2,4-Trimethylbenzene	0.0079	N/A	N/A	120.1900	0.0100	0.0370	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene	0.6081	N/A	N/A	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene	0.0478	N/A	N/A	106.1700	0.0001	0.0029	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)	1.0380	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene	0.1586	N/A	N/A	92.1300	0.0003	0.0237	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components	0.0027	N/A	N/A	134.1368	0.9866	0.8802	189.60	
Xylene (-m)	0.0395	N/A	N/A	106.1700	0.0029	0.0534	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	0.1253	0.1253	0.1395	0.1655	0.1954	0.2254	0.2465	0.2396	0.2090	0.1748	0.1479	0.1253
Seal Factor A (lb-mole/ft-yr):	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0031	0.0035	0.0041	0.0048	0.0056	0.0061	0.0059	0.0052	0.0043	0.0037	0.0031
Tank Diameter (ft):	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	7.7956	6.9582	5.1939	8.4465	9.0201	6.8405	8.6160	10.6743	6.2326	9.7955	8.7216	10.1200
Number of Columns:	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000	9.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	4,191,071.000	3,740,881.000	2,792,353.000	4,541,026.000	4,849,401.000	3,677,578.000	4,632,133.000	5,738,750.000	3,350,766.000	5,266,247.000	4,688,923.000	5,440,710.000
	0	0	0	0	0	0	0	0	0	0	0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000
Tank Diameter (ft):	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000
Deck Fitting Losses (lb):	0.1145	0.1145	0.1275	0.1512	0.1785	0.2060	0.2252	0.2189	0.1910	0.1597	0.1351	0.1145
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	200.3000	200.3000	200.3000	200.3000	200.3000	200.3000	200.3000	200.3000	200.3000	200.3000	200.3000	200.3000
Deck Seam Losses (lb):	0.3004	0.3004	0.3344	0.3968	0.4684	0.5404	0.5909	0.5744	0.5011	0.4191	0.3546	0.3004
Deck Seam Length (ft):	2,948.2300	2,948.2300	2,948.2300	2,948.2300	2,948.2300	2,948.2300	2,948.2300	2,948.2300	2,948.2300	2,948.2300	2,948.2300	2,948.2300
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400	0.1400
Deck Seam Length Factor(ft/sqft):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Tank Diameter (ft):	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000	137.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Unbolted Cover, Ungasketed	1	36.00	5.90	1.20	0.3487
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Ungask.	1	47.00	0.00	0.00	0.4552
Ladder Well (36-in. Diam.)/Sliding Cover, Ungasketed	1	76.00	0.00	0.00	0.7361
Roof Leg or Hanger Well/Adjustable	1	7.90	0.00	0.00	0.0765
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1	12.00	0.00	0.00	0.1162
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	0.0601
Stub Drain (1-in. Diameter)/	1	1.20	0.00	0.00	0.0116
Automatic Gauge Float Well/Unbolted Cover, Ungasketed	1	14.00	5.40	1.10	0.1356

Total Losses (lb):	8.3358	7.4984	5.7952	9.1601	9.8624	7.8122	9.6786	11.7072	7.1336	10.5490	9.3592	10.6602

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Distillate fuel oil no. 2	2.12	98.41	1.94	5.08	107.55
1,2,4-Trimethylbenzene	0.09	0.98	0.08	0.21	1.36
Benzene	0.00	0.00	0.00	0.01	0.02
Ethylbenzene	0.01	0.01	0.01	0.02	0.04
Hexane (-n)	0.00	0.00	0.00	0.00	0.00
Toluene	0.05	0.03	0.05	0.12	0.25
Unidentified Components	1.85	97.10	1.69	4.44	105.08
Xylene (-m)	0.12	0.29	0.11	0.29	0.80

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002007-A
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Internal Floating Roof Tank
Description:	2005 Operations

Tank Dimensions

Diameter (ft):	132.00
Volume (gallons):	5,670,000.00
Turnovers:	1.87
Self Supp. Roof? (y/n):	N
No. of Columns:	8.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Vapor-mounted
Secondary Seal:	None

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Welded

Deck Fitting/Status	Quantity
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	2
Automatic Gauge Float Well/Bolted Cover, Gasketed	1
Column Well (24-in. Diam.)/Pipe Col.-Sliding Cover, Gask.	1
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.	1

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Jet kerosene	Jan	35.40	31.29	39.51	45.40	0.0041	N/A	N/A	130.0000			162.00	Option 1: VP40 = .0041
1,2,4-Trimethylbenzene						0.0072	N/A	N/A	120.1900	0.0250	0.0543	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5661	N/A	N/A	78.1100	0.0180	3.0972	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.5974	N/A	N/A	84.1600	0.0024	0.4358	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0436	N/A	N/A	106.1700	0.0140	0.1857	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						0.9706	N/A	N/A	86.1700	0.0100	2.9501	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	2.5896	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0192	N/A	N/A	120.2000	0.0050	0.0291	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.1200	70.0278	88.15	Option 1: VP40 = 1.92
Toluene						0.1464	N/A	N/A	92.1300	0.0700	3.1141	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-1.3414	N/A	N/A	88.2584	0.6256	-82.2505	273.70	
Xylene (-m)						0.0360	N/A	N/A	106.1700	0.0700	0.7668	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Feb	36.87	32.28	41.45	45.40	0.0041	N/A	N/A	130.0000			162.00	Option 1: VP40 = .0041
1,2,4-Trimethylbenzene						0.0076	N/A	N/A	120.1900	0.0250	0.0581	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5926	N/A	N/A	78.1100	0.0180	3.2421	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.6247	N/A	N/A	84.1600	0.0024	0.4557	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0462	N/A	N/A	106.1700	0.0140	0.1968	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0131	N/A	N/A	86.1700	0.0100	3.0792	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	2.5896	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0204	N/A	N/A	120.2000	0.0050	0.0310	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.1200	70.0278	88.15	Option 1: VP40 = 1.92
Toluene						0.1541	N/A	N/A	92.1300	0.0700	3.2783	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-1.3500	N/A	N/A	88.2531	0.6256	-82.7710	273.70	
Xylene (-m)						0.0382	N/A	N/A	106.1700	0.0700	0.8127	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Mar	41.56	37.07	46.06	45.40	0.0044	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0094	N/A	N/A	120.1900	0.0250	0.0671	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6843	N/A	N/A	78.1100	0.0180	3.5093	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.7189	N/A	N/A	84.1600	0.0024	0.4915	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0554	N/A	N/A	106.1700	0.0140	0.2211	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1593	N/A	N/A	86.1700	0.0100	3.3028	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2402	N/A	N/A	114.2200	0.0400	2.7371	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0248	N/A	N/A	120.2000	0.0050	0.0353	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.0106	N/A	N/A	88.1500	0.1200	68.7389	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.1811	N/A	N/A	92.1300	0.0700	3.6122	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-1.4372	N/A	N/A	88.2874	0.6256	-82.6300	273.70	
Xylene (-m)						0.0459	N/A	N/A	106.1700	0.0700	0.9146	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Apr	46.44	41.38	51.49	45.40	0.0052	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0116	N/A	N/A	120.1900	0.0250	0.0699	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7918	N/A	N/A	78.1100	0.0180	3.4203	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.8289	N/A	N/A	84.1600	0.0024	0.4774	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0666	N/A	N/A	106.1700	0.0140	0.2238	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3292	N/A	N/A	86.1700	0.0100	3.1896	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.3250	N/A	N/A	114.2200	0.0400	3.1195	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0302	N/A	N/A	120.2000	0.0050	0.0363	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.2933	N/A	N/A	88.1500	0.1200	66.0386	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.2134	N/A	N/A	92.1300	0.0700	3.5845	92.13	Option 2: A=6.954, B=1344.8, C=219.48

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Unidentified Components						-1.6515	N/A	N/A	88.4072	0.6256	-80.0871	273.70	
Xylene (-m)						0.0552	N/A	N/A	106.1700	0.0700	0.9273	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	May	51.25	45.58	56.92	45.40	0.0061	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0143	N/A	N/A	120.1900	0.0250	0.0725	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9115	N/A	N/A	78.1100	0.0180	3.3342	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.9510	N/A	N/A	84.1600	0.0024	0.4638	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0795	N/A	N/A	106.1700	0.0140	0.2262	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.5166	N/A	N/A	86.1700	0.0100	3.0820	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4111	N/A	N/A	114.2200	0.0400	3.3416	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0366	N/A	N/A	120.2000	0.0050	0.0371	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.5899	N/A	N/A	88.1500	0.1200	63.1561	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2499	N/A	N/A	92.1300	0.0700	3.5554	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-1.8783	N/A	N/A	88.4938	0.6256	-77.2080	273.70	
Xylene (-m)						0.0660	N/A	N/A	106.1700	0.0700	0.9389	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Jun	55.47	49.47	61.48	45.40	0.0071	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0170	N/A	N/A	120.1900	0.0250	0.0749	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.0287	N/A	N/A	78.1100	0.0180	3.2601	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.0702	N/A	N/A	84.1600	0.0024	0.4522	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0925	N/A	N/A	106.1700	0.0140	0.2281	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6987	N/A	N/A	86.1700	0.0100	2.9909	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4926	N/A	N/A	114.2200	0.0400	3.4695	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0431	N/A	N/A	120.2000	0.0050	0.0379	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.8941	N/A	N/A	88.1500	0.1200	61.1462	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2863	N/A	N/A	92.1300	0.0700	3.5285	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-2.1084	N/A	N/A	88.5542	0.6256	-75.1367	273.70	
Xylene (-m)						0.0769	N/A	N/A	106.1700	0.0700	0.9483	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Jul	58.15	52.19	64.11	45.40	0.0077	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0190	N/A	N/A	120.1900	0.0250	0.0763	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1092	N/A	N/A	78.1100	0.0180	3.2139	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.1520	N/A	N/A	84.1600	0.0024	0.4450	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.1017	N/A	N/A	106.1700	0.0140	0.2293	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.8232	N/A	N/A	86.1700	0.0100	2.9347	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.5443	N/A	N/A	114.2200	0.0400	3.5047	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0477	N/A	N/A	120.2000	0.0050	0.0384	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						3.0868	N/A	N/A	88.1500	0.1200	59.6262	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.3116	N/A	N/A	92.1300	0.0700	3.5109	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-2.2561	N/A	N/A	88.5830	0.6256	-73.5333	273.70	
Xylene (-m)						0.0847	N/A	N/A	106.1700	0.0700	0.9540	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Aug	57.30	51.62	62.97	45.40	0.0075	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0183	N/A	N/A	120.1900	0.0250	0.0759	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.0829	N/A	N/A	78.1100	0.0180	3.2286	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.1253	N/A	N/A	84.1600	0.0024	0.4473	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0987	N/A	N/A	106.1700	0.0140	0.2289	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.7826	N/A	N/A	86.1700	0.0100	2.9525	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.5278	N/A	N/A	114.2200	0.0400	3.4968	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0462	N/A	N/A	120.2000	0.0050	0.0382	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						3.0253	N/A	N/A	88.1500	0.1200	60.1286	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.3033	N/A	N/A	92.1300	0.0700	3.5166	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-2.2087	N/A	N/A	88.5745	0.6256	-74.0656	273.70	
Xylene (-m)						0.0821	N/A	N/A	106.1700	0.0700	0.9522	106.17	Option 2: A=7.009, B=1462.266, C=215.11

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Jet kerosene	Sep	53.23	47.96	58.50	45.40	0.0066	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0155	N/A	N/A	120.1900	0.0250	0.0736	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9651	N/A	N/A	78.1100	0.0180	3.2993	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						1.0055	N/A	N/A	84.1600	0.0024	0.4584	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0854	N/A	N/A	106.1700	0.0140	0.2271	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6000	N/A	N/A	86.1700	0.0100	3.0389	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.4494	N/A	N/A	114.2200	0.0400	3.4140	114.22	Option 1: VP50 = .387 VP60 = .58
Isopropyl benzene						0.0395	N/A	N/A	120.2000	0.0050	0.0375	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.7327	N/A	N/A	88.1500	0.1200	62.2822	88.15	Option 1: VP50 = 2.5 VP60 = 3.22
Toluene						0.2665	N/A	N/A	92.1300	0.0700	3.5429	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-1.9858	N/A	N/A	88.5247	0.6256	-76.3172	273.70	
Xylene (-m)						0.0710	N/A	N/A	106.1700	0.0700	0.9434	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Oct	48.01	43.23	52.78	45.40	0.0055	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0125	N/A	N/A	120.1900	0.0250	0.0707	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8294	N/A	N/A	78.1100	0.0180	3.3920	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.8673	N/A	N/A	84.1600	0.0024	0.4729	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0706	N/A	N/A	106.1700	0.0140	0.2246	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3882	N/A	N/A	86.1700	0.0100	3.1540	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.3523	N/A	N/A	114.2200	0.0400	3.2022	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0322	N/A	N/A	120.2000	0.0050	0.0365	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.3845	N/A	N/A	88.1500	0.1200	65.0116	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.2248	N/A	N/A	92.1300	0.0700	3.5752	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-1.7216	N/A	N/A	88.4378	0.6256	-79.0709	273.70	
Xylene (-m)						0.0585	N/A	N/A	106.1700	0.0700	0.9312	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Nov	43.22	39.55	46.89	45.40	0.0046	N/A	N/A	130.0000			162.00	Option 5: A=12.39, B=8933
1,2,4-Trimethylbenzene						0.0101	N/A	N/A	120.1900	0.0250	0.0680	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7194	N/A	N/A	78.1100	0.0180	3.4789	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.7548	N/A	N/A	84.1600	0.0024	0.4867	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0590	N/A	N/A	106.1700	0.0140	0.2220	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.2149	N/A	N/A	86.1700	0.0100	3.2638	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2690	N/A	N/A	114.2200	0.0400	2.8909	114.22	Option 1: VP40 = .213 VP50 = .387
Isopropyl benzene						0.0265	N/A	N/A	120.2000	0.0050	0.0356	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						2.1067	N/A	N/A	88.1500	0.1200	67.9167	88.15	Option 1: VP40 = 1.92 VP50 = 2.5
Toluene						0.1916	N/A	N/A	92.1300	0.0700	3.6030	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-1.5096	N/A	N/A	88.3330	0.6256	-81.8847	273.70	
Xylene (-m)						0.0489	N/A	N/A	106.1700	0.0700	0.9190	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Dec	37.70	34.02	41.39	45.40	0.0041	N/A	N/A	130.0000			162.00	Option 1: VP40 = .0041
1,2,4-Trimethylbenzene						0.0079	N/A	N/A	120.1900	0.0250	0.0603	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6081	N/A	N/A	78.1100	0.0180	3.3271	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Cyclohexane						0.6407	N/A	N/A	84.1600	0.0024	0.4673	84.16	Option 2: A=6.841, B=1201.53, C=222.65
Ethylbenzene						0.0478	N/A	N/A	106.1700	0.0140	0.2033	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0380	N/A	N/A	86.1700	0.0100	3.1547	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Isooctane						0.2130	N/A	N/A	114.2200	0.0400	2.5896	114.22	Option 1: VP40 = .213
Isopropyl benzene						0.0211	N/A	N/A	120.2000	0.0050	0.0321	120.20	Option 2: A=6.963, B=1460.793, C=207.78
Methyl-tert-butyl ether (MTBE)						1.9200	N/A	N/A	88.1500	0.1200	70.0278	88.15	Option 1: VP40 = 1.92
Toluene						0.1586	N/A	N/A	92.1300	0.0700	3.3750	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						-1.3550	N/A	N/A	88.2502	0.6256	-83.0770	273.70	
Xylene (-m)						0.0395	N/A	N/A	106.1700	0.0700	0.8399	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	0.6687	0.6687	0.7134	0.8470	1.0002	1.1544	1.2628	1.2272	1.0702	0.8946	0.7565	0.6687
Seal Factor A (lb-mole/ft-yr):	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0041	0.0041	0.0044	0.0052	0.0061	0.0071	0.0077	0.0075	0.0066	0.0055	0.0046	0.0041
Tank Diameter (ft):	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	5.2783	6.3352	0.0000	4.4972	3.9619	0.0000
Number of Columns:	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	2,786,530.000	3,344,497.000	0.0000	2,374,184.000	2,091,565.000	0.0000
							0	0		0	0	
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000	7.0000
Tank Diameter (ft):	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000
Deck Fitting Losses (lb):	0.0560	0.0560	0.0597	0.0709	0.0837	0.0966	0.1057	0.1027	0.0895	0.0749	0.0633	0.0560
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	74.0000	74.0000	74.0000	74.0000	74.0000	74.0000	74.0000	74.0000	74.0000	74.0000	74.0000	74.0000
Deck Seam Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length Factor(ft/sqft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tank Diameter (ft):	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	KFa (lb-mole/yr)	Deck Fitting Loss Factors KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed	2	1.60	0.00	0.00	0.0396
Automatic Gauge Float Well/Bolted Cover, Gasketed	1	2.80	0.00	0.00	0.0347
Column Well (24-in. Diam.)/Pipe Col.-Sliding Cover, Gask.	1	25.00	0.00	0.00	0.3095
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.	1	43.00	0.00	0.00	0.5324

Total Losses (lb):	0.7246	0.7246	0.7731	0.9178	1.0839	1.2510	6.6467	7.6651	1.1597	5.4667	4.7817	0.7246

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Jet kerosene	10.93	20.07	0.91	0.00	31.92
1,2,4-Trimethylbenzene	0.76	0.50	0.06	0.00	1.33
Benzene	36.18	0.36	3.03	0.00	39.57
Cyclohexane	5.04	0.05	0.42	0.00	5.51
Ethylbenzene	2.41	0.28	0.20	0.00	2.89
Hexane (-n)	33.61	0.20	2.81	0.00	36.62
Isooctane	34.56	0.80	2.89	0.00	38.25
Isopropyl benzene	0.39	0.10	0.03	0.00	0.53
Methyl-tert-butyl ether (MTBE)	704.48	2.41	58.95	0.00	765.83
Toluene	38.24	1.41	3.20	0.00	42.84
Unidentified Components	-854.74	12.56	-71.52	0.00	-913.70
Xylene (-m)	10.00	1.41	0.84	0.00	12.24

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002008-B
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Internal Floating Roof Tank
Description:	2005 Operations

Tank Dimensions

Diameter (ft):	132.00
Volume (gallons):	5,670,000.00
Turnovers:	3.75
Self Supp. Roof? (y/n):	N
No. of Columns:	8.00
Eff. Col. Diam. (ft):	1.00

Paint Characteristics

Internal Shell Condition:	Light Rust
Shell Color/Shade:	White/White
Shell Condition:	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Rim-Seal System

Primary Seal:	Vapor-mounted
Secondary Seal:	None

Deck Characteristics

Deck Fitting Category:	Detail
Deck Type:	Welded

Deck Fitting/Status	Quantity
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1
Roof Leg or Hanger Well/Adjustable	1
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Ungask.	1
Automatic Gauge Float Well/Unbolted Cover, Ungasketed	1
Access Hatch (24-in. Diam.)/Unbolted Cover, Ungasketed	2

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	35.40	31.29	39.51	45.40	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031
1,2,4-Trimethylbenzene						0.0072	N/A	N/A	120.1900	0.0100	0.0334	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5661	N/A	N/A	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0436	N/A	N/A	106.1700	0.0001	0.0026	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						0.9706	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1464	N/A	N/A	92.1300	0.0003	0.0219	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	N/A	N/A	133.7346	0.9866	0.8908	189.60	
Xylene (-m)						0.0360	N/A	N/A	106.1700	0.0029	0.0488	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Feb	36.87	32.28	41.45	45.40	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031
1,2,4-Trimethylbenzene						0.0076	N/A	N/A	120.1900	0.0100	0.0357	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.5926	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0462	N/A	N/A	106.1700	0.0001	0.0028	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0131	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1541	N/A	N/A	92.1300	0.0003	0.0230	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	N/A	N/A	133.9859	0.9866	0.8842	189.60	
Xylene (-m)						0.0382	N/A	N/A	106.1700	0.0029	0.0517	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Mar	41.56	37.07	46.06	45.40	0.0035	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0094	N/A	N/A	120.1900	0.0100	0.0395	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6843	N/A	N/A	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0554	N/A	N/A	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1593	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1811	N/A	N/A	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0030	N/A	N/A	134.3258	0.9866	0.8747	189.60	
Xylene (-m)						0.0459	N/A	N/A	106.1700	0.0029	0.0557	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Apr	46.44	41.38	51.49	45.40	0.0041	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0116	N/A	N/A	120.1900	0.0100	0.0411	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7918	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0666	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3292	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2134	N/A	N/A	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0035	N/A	N/A	134.3696	0.9866	0.8725	189.60	
Xylene (-m)						0.0552	N/A	N/A	106.1700	0.0029	0.0565	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	May	51.25	45.58	56.92	45.40	0.0048	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0143	N/A	N/A	120.1900	0.0100	0.0427	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9115	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0795	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.5166	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2499	N/A	N/A	92.1300	0.0003	0.0239	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0042	N/A	N/A	134.4098	0.9866	0.8703	189.60	
Xylene (-m)						0.0660	N/A	N/A	106.1700	0.0029	0.0573	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jun	55.47	49.47	61.48	45.40	0.0056	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0170	N/A	N/A	120.1900	0.0100	0.0441	120.19	Option 2: A=7.04383, B=1573.267, C=208.56

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Benzene						1.0287	N/A	N/A	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0925	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6987	N/A	N/A	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2863	N/A	N/A	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0048	N/A	N/A	134.4425	0.9866	0.8686	189.60	
Xylene (-m)						0.0769	N/A	N/A	106.1700	0.0029	0.0579	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jul	58.15	52.19	64.11	45.40	0.0061	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0190	N/A	N/A	120.1900	0.0100	0.0450	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1092	N/A	N/A	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1017	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.8232	N/A	N/A	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3116	N/A	N/A	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0052	N/A	N/A	134.4620	0.9866	0.8675	189.60	
Xylene (-m)						0.0847	N/A	N/A	106.1700	0.0029	0.0582	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Aug	57.30	51.62	62.97	45.40	0.0059	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0183	N/A	N/A	120.1900	0.0100	0.0447	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.0829	N/A	N/A	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0987	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.7826	N/A	N/A	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3033	N/A	N/A	92.1300	0.0003	0.0237	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0051	N/A	N/A	134.4559	0.9866	0.8678	189.60	
Xylene (-m)						0.0821	N/A	N/A	106.1700	0.0029	0.0581	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Sep	53.23	47.96	58.50	45.40	0.0052	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0155	N/A	N/A	120.1900	0.0100	0.0434	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9651	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0854	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6000	N/A	N/A	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2665	N/A	N/A	92.1300	0.0003	0.0239	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0044	N/A	N/A	134.4254	0.9866	0.8695	189.60	
Xylene (-m)						0.0710	N/A	N/A	106.1700	0.0029	0.0576	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Oct	48.01	43.23	52.78	45.40	0.0043	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0125	N/A	N/A	120.1900	0.0100	0.0416	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8294	N/A	N/A	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0706	N/A	N/A	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3882	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2248	N/A	N/A	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0037	N/A	N/A	134.3831	0.9866	0.8718	189.60	
Xylene (-m)						0.0585	N/A	N/A	106.1700	0.0029	0.0568	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Nov	43.22	39.55	46.89	45.40	0.0037	N/A	N/A	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0101	N/A	N/A	120.1900	0.0100	0.0400	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.7194	N/A	N/A	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0590	N/A	N/A	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.2149	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1916	N/A	N/A	92.1300	0.0003	0.0242	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0032	N/A	N/A	134.3410	0.9866	0.8739	189.60	
Xylene (-m)						0.0489	N/A	N/A	106.1700	0.0029	0.0560	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Dec	37.70	34.02	41.39	45.40	0.0031	N/A	N/A	130.0000			188.00	Option 1: VP40 = .0031

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

1,2,4-Trimethylbenzene	0.0079	N/A	N/A	120.1900	0.0100	0.0370	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene	0.6081	N/A	N/A	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene	0.0478	N/A	N/A	106.1700	0.0001	0.0029	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)	1.0380	N/A	N/A	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene	0.1586	N/A	N/A	92.1300	0.0003	0.0237	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components	0.0027	N/A	N/A	134.1368	0.9866	0.8802	189.60	
Xylene (-m)	0.0395	N/A	N/A	106.1700	0.0029	0.0534	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Rim Seal Losses (lb):	0.5056	0.5056	0.5628	0.6678	0.7882	0.9094	0.9945	0.9666	0.8432	0.7052	0.5967	0.5056
Seal Factor A (lb-mole/ft-yr):	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000	6.7000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000	0.2000
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0031	0.0035	0.0041	0.0048	0.0056	0.0061	0.0059	0.0052	0.0043	0.0037	0.0031
Tank Diameter (ft):	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Withdrawal Losses (lb):	5.2575	2.3129	8.4811	6.9450	0.0000	0.0000	8.9977	0.0000	0.0000	0.0000	6.7633	2.0426
Number of Columns:	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	2,736,422.000	1,203,845.000	4,414,263.000	3,614,751.000	0.0000	0.0000	4,683,160.000	0.0000	0.0000	0.0000	3,520,200.000	1,063,167.000
	0	0	0	0			0				0	0
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
Average Organic Liquid Density (lb/gal):	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000	7.1000
Tank Diameter (ft):	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000
Deck Fitting Losses (lb):	0.0909	0.0909	0.1012	0.1201	0.1418	0.1636	0.1789	0.1739	0.1517	0.1269	0.1073	0.0909
Value of Vapor Pressure Function:	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	159.1000	159.1000	159.1000	159.1000	159.1000	159.1000	159.1000	159.1000	159.1000	159.1000	159.1000	159.1000
Deck Seam Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Loss per Unit Length Factor (lb-mole/ft-yr):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length Factor(ft/sqft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tank Diameter (ft):	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000	132.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000

Deck Fitting/Status	Quantity	Deck Fitting Loss Factors KFa (lb-mole/yr)	KFb (lb-mole/(yr mph^n))	m	Losses (lb.)
Vacuum Breaker (10-in. Diam.)/Weighted Mech. Actuation, Gask.	1	6.20	1.20	0.94	0.0601
Sample Pipe or Well (24-in. Diam.)/Slit Fabric Seal 10% Open	1	12.00	0.00	0.00	0.1162
Roof Leg or Hanger Well/Adjustable	1	7.90	0.00	0.00	0.0765
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Ungask.	1	47.00	0.00	0.00	0.4552
Automatic Gauge Float Well/Unbolted Cover, Ungasketed	1	14.00	5.40	1.10	0.1356
Access Hatch (24-in. Diam.)/Unbolted Cover, Ungasketed	2	36.00	5.90	1.20	0.6974

Total Losses (lb):	5.8540	2.9095	9.1451	7.7329	0.9300	1.0730	10.1711	1.1404	0.9949	0.8321	7.4674	2.6392

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)				
Components	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Distillate fuel oil no. 2	8.55	40.80	1.54	0.00	50.89
1,2,4-Trimethylbenzene	0.35	0.41	0.06	0.00	0.83
Benzene	0.02	0.00	0.00	0.00	0.02
Ethylbenzene	0.03	0.01	0.00	0.00	0.04
Hexane (-n)	0.00	0.00	0.00	0.00	0.00
Toluene	0.20	0.01	0.04	0.00	0.25
Unidentified Components	7.46	40.26	1.34	0.00	49.06
Xylene (-m)	0.48	0.12	0.09	0.00	0.69

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002009
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Vertical Fixed Roof Tank
Description:	2005 Operations-Not operational during 2005. No emissions from this tank during 2005.

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	140.00
Liquid Height (ft):	40.00
Avg. Liquid Height (ft):	20.00
Volume (gallons):	4,620,000.00
Turnovers:	0.00
Net Throughput (gal/yr):	0.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	Gray/Medium
Shell Condition:	Good
Roof Color/Shade:	Gray/Medium
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	4.38
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	0.00
Pressure Settings (psig):	0.00

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	39.52	33.27	45.76	48.46	0.0031	0.0031	0.0040	130.0000			188.00	Option 1: VP40 = .0031
1,2,4-Trimethylbenzene						0.0086	0.0065	0.0113	120.1900	0.0100	0.0402	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6430	0.5296	0.7762	78.1100	0.0000	0.0024	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0512	0.0401	0.0650	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0936	0.9118	1.3045	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1689	0.1358	0.2087	92.1300	0.0003	0.0252	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	0.0024	0.0025	134.4854	0.9866	0.8713	189.60	
Xylene (-m)						0.0424	0.0331	0.0538	106.1700	0.0029	0.0573	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Feb	42.16	34.40	49.91	48.46	0.0035	0.0031	0.0046	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0097	0.0068	0.0135	120.1900	0.0100	0.0397	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6968	0.5487	0.8769	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0567	0.0420	0.0757	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1791	0.9427	1.4626	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1848	0.1413	0.2393	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0030	0.0027	0.0029	134.3313	0.9866	0.8744	189.60	
Xylene (-m)						0.0469	0.0346	0.0628	106.1700	0.0029	0.0558	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Mar	48.20	39.34	57.05	48.46	0.0044	0.0031	0.0059	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0126	0.0085	0.0181	120.1900	0.0100	0.0417	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8340	0.6395	1.0756	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0711	0.0509	0.0979	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3954	1.0881	1.7713	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2262	0.1679	0.3010	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0038	0.0033	0.0035	134.3847	0.9866	0.8717	189.60	
Xylene (-m)						0.0590	0.0421	0.0814	106.1700	0.0029	0.0568	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Apr	54.16	43.78	64.54	48.46	0.0053	0.0037	0.0075	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0161	0.0104	0.0245	120.1900	0.0100	0.0437	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9911	0.7317	1.3229	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0883	0.0603	0.1269	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6404	1.2343	2.1508	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2746	0.1953	0.3797	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0046	0.0040	0.0042	134.4326	0.9866	0.8691	189.60	
Xylene (-m)						0.0734	0.0499	0.1058	106.1700	0.0029	0.0577	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	May	60.08	48.11	72.06	48.46	0.0065	0.0043	0.0096	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0205	0.0125	0.0327	120.1900	0.0100	0.0456	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1705	0.8318	1.6167	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1088	0.0709	0.1632	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9175	1.3919	2.5963	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3310	0.2255	0.4756	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0056	0.0048	0.0050	134.4755	0.9866	0.8667	189.60	
Xylene (-m)						0.0906	0.0588	0.1364	106.1700	0.0029	0.0585	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jun	64.97	52.07	77.87	48.46	0.0076	0.0050	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0249	0.0148	0.0406	120.1900	0.0100	0.0472	120.19	Option 2: A=7.04383, B=1573.267, C=208.56

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Benzene						1.3383	0.9333	1.8792	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1288	0.0819	0.1970	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.1743	1.5506	2.9903	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3847	0.2567	0.5631	92.1300	0.0003	0.0233	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0065	0.0056	0.0058	134.5075	0.9866	0.8648	189.60	
Xylene (-m)						0.1074	0.0680	0.1651	106.1700	0.0029	0.0591	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jul	67.56	54.78	80.34	48.46	0.0083	0.0054	0.0124	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0275	0.0165	0.0444	120.1900	0.0100	0.0480	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.4350	1.0086	2.0008	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1405	0.0903	0.2131	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.3214	1.6676	3.1718	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.4160	0.2800	0.6042	92.1300	0.0003	0.0232	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0071	0.0061	0.0063	134.5233	0.9866	0.8638	189.60	
Xylene (-m)						0.1173	0.0750	0.1787	106.1700	0.0029	0.0594	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Aug	65.85	54.11	77.60	48.46	0.0078	0.0053	0.0114	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0257	0.0161	0.0402	120.1900	0.0100	0.0475	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.3707	0.9897	1.8660	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1327	0.0882	0.1953	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.2237	1.6382	2.9706	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3952	0.2741	0.5587	92.1300	0.0003	0.0233	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0067	0.0058	0.0061	134.5130	0.9866	0.8644	189.60	
Xylene (-m)						0.1107	0.0733	0.1636	106.1700	0.0029	0.0592	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Sep	60.36	50.29	70.42	48.46	0.0066	0.0047	0.0091	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0207	0.0137	0.0307	120.1900	0.0100	0.0457	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1795	0.8866	1.5486	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1099	0.0768	0.1546	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9313	1.4777	2.4935	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3338	0.2423	0.4532	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0056	0.0049	0.0052	134.4774	0.9866	0.8666	189.60	
Xylene (-m)						0.0915	0.0637	0.1292	106.1700	0.0029	0.0585	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Oct	53.46	45.37	61.54	48.46	0.0052	0.0039	0.0068	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0157	0.0111	0.0217	120.1900	0.0100	0.0435	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9713	0.7673	1.2187	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0861	0.0640	0.1145	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6097	1.2904	1.9915	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2684	0.2060	0.3463	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0045	0.0040	0.0042	134.4272	0.9866	0.8694	189.60	
Xylene (-m)						0.0715	0.0530	0.0954	106.1700	0.0029	0.0576	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Nov	47.24	41.53	52.95	48.46	0.0042	0.0034	0.0051	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0120	0.0094	0.0153	120.1900	0.0100	0.0414	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8108	0.6836	0.9572	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0686	0.0554	0.0845	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3589	1.1581	1.5877	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2191	0.1809	0.2640	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0036	0.0033	0.0035	134.3765	0.9866	0.8721	189.60	
Xylene (-m)						0.0569	0.0458	0.0702	106.1700	0.0029	0.0567	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Dec	41.35	35.95	46.74	48.46	0.0034	0.0031	0.0041	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

1,2,4-Trimethylbenzene	0.0093	0.0073	0.0118	120.1900	0.0100	0.0394	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene	0.6799	0.5760	0.7990	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene	0.0550	0.0446	0.0674	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)	1.1522	0.9865	1.3404	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene	0.1798	0.1492	0.2156	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components	0.0030	0.0027	0.0028	134.3238	0.9866	0.8748	189.60	
Xylene (-m)	0.0455	0.0368	0.0558	106.1700	0.0029	0.0557	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	38.4573	48.5296	73.9890	100.4345	142.4774	170.9151	188.2417	164.7999	116.8202	79.1529	44.8194	36.4241
Vapor Space Volume (cu ft):	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001
Vapor Space Expansion Factor:	0.0501	0.0619	0.0699	0.0811	0.0925	0.0988	0.0974	0.0898	0.0777	0.0632	0.0452	0.0431
Vented Vapor Saturation Factor:	0.9965	0.9960	0.9951	0.9940	0.9927	0.9914	0.9907	0.9912	0.9926	0.9941	0.9952	0.9961
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772	330,325.3772
Tank Diameter (ft):	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000
Vapor Space Outage (ft):	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000
Roof Outage (ft):	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583
Roof Outage (Cone Roof)												
Roof Outage (ft):	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583	1.4583
Roof Height (ft):	4.3750	4.3750	4.3750	4.3750	4.3750	4.3750	4.3750	4.3750	4.3750	4.3750	4.3750	4.3750
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	70.0000	70.0000	70.0000	70.0000	70.0000	70.0000	70.0000	70.0000	70.0000	70.0000	70.0000	70.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Daily Avg. Liquid Surface Temp. (deg. R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Average Ambient Temp. (deg. F):	20.8500	23.3000	32.9500	43.2000	53.3000	62.4000	68.5500	67.2500	59.1000	48.5000	38.7000	26.4500
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292
Tank Paint Solar Absorptance (Shell):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Tank Paint Solar Absorptance (Roof):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Daily Total Solar Insulation Factor (Btu/sqft day):	597.1021	888.0387	1,221.4895	1,492.4381	1,767.1939	1,931.5398	1,909.9654	1,698.9809	1,343.3212	927.0629	571.7205	478.7604
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0501	0.0619	0.0699	0.0811	0.0925	0.0988	0.0974	0.0898	0.0777	0.0632	0.0452	0.0431
Daily Vapor Temperature Range (deg. R):	24.9768	31.0203	35.4252	41.5200	47.9034	51.6085	51.1257	46.9646	40.2648	32.3393	22.8376	21.5716
Daily Vapor Pressure Range (psia):	0.0009	0.0015	0.0028	0.0038	0.0052	0.0065	0.0069	0.0060	0.0044	0.0029	0.0017	0.0010
Breather Vent Press. Setting Range(psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0031	0.0031	0.0031	0.0037	0.0043	0.0050	0.0054	0.0053	0.0047	0.0039	0.0034	0.0031
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0040	0.0046	0.0059	0.0075	0.0096	0.0115	0.0124	0.0114	0.0091	0.0068	0.0051	0.0041
Daily Avg. Liquid Surface Temp. (deg R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Min. Liquid Surface Temp. (deg R):	492.9446	494.0746	499.0107	503.4525	507.7767	511.7372	514.4480	513.7829	509.9612	505.0425	501.1970	495.6241
Daily Max. Liquid Surface Temp. (deg R):	505.4330	509.5847	516.7233	524.2125	531.7283	537.5415	540.0109	537.2652	530.0937	521.2121	512.6158	506.4099
Daily Ambient Temp. Range (deg. R):	18.9000	19.6000	16.9000	18.2000	19.8000	20.6000	20.5000	20.3000	20.4000	20.4000	16.6000	17.3000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9965	0.9960	0.9951	0.9940	0.9927	0.9914	0.9907	0.9912	0.9926	0.9941	0.9952	0.9961
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Vapor Space Outage (ft):	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583	21.4583

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Net Throughput (gal/mo.):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Annual Turnovers:	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000	4,620,000,000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Tank Diameter (ft):	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000	140.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	38.4573	48.5296	73.9890	100.4345	142.4774	170.9151	188.2417	164.7999	116.8202	79.1529	44.8194	36.4241

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	0.00	1,205.06	1,205.06
1,2,4-Trimethylbenzene	0.00	54.43	54.43
Benzene	0.00	2.53	2.53
Ethylbenzene	0.00	3.78	3.78
Hexane (-n)	0.00	0.52	0.52
Toluene	0.00	28.49	28.49
Unidentified Components	0.00	1,045.07	1,045.07
Xylene (-m)	0.00	70.24	70.24

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002010
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Vertical Fixed Roof Tank
Description:	2005 Operations-Not operational during 2005. No emissions from this tank during 2005.

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	100.00
Liquid Height (ft):	39.00
Avg. Liquid Height (ft):	20.00
Volume (gallons):	2,100,000.00
Turnovers:	0.00
Net Throughput (gal/yr):	0.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	Gray/Medium
Shell Condition:	Good
Roof Color/Shade:	Gray/Medium
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	3.13
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	0.00
Pressure Settings (psig):	0.00

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	39.52	33.27	45.76	48.46	0.0031	0.0031	0.0040	130.0000			188.00	Option 1: VP40 = .0031
1,2,4-Trimethylbenzene						0.0086	0.0065	0.0113	120.1900	0.0100	0.0402	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6430	0.5296	0.7762	78.1100	0.0000	0.0024	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0512	0.0401	0.0650	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0936	0.9118	1.3045	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1689	0.1358	0.2087	92.1300	0.0003	0.0252	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	0.0024	0.0025	134.4854	0.9866	0.8713	189.60	
Xylene (-m)						0.0424	0.0331	0.0538	106.1700	0.0029	0.0573	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Feb	42.16	34.40	49.91	48.46	0.0035	0.0031	0.0046	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0097	0.0068	0.0135	120.1900	0.0100	0.0397	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6968	0.5487	0.8769	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0567	0.0420	0.0757	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1791	0.9427	1.4626	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1848	0.1413	0.2393	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0030	0.0027	0.0029	134.3313	0.9866	0.8744	189.60	
Xylene (-m)						0.0469	0.0346	0.0628	106.1700	0.0029	0.0558	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Mar	48.20	39.34	57.05	48.46	0.0044	0.0031	0.0059	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0126	0.0085	0.0181	120.1900	0.0100	0.0417	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8340	0.6395	1.0756	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0711	0.0509	0.0979	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3954	1.0881	1.7713	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2262	0.1679	0.3010	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0038	0.0033	0.0035	134.3847	0.9866	0.8717	189.60	
Xylene (-m)						0.0590	0.0421	0.0814	106.1700	0.0029	0.0568	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Apr	54.16	43.78	64.54	48.46	0.0053	0.0037	0.0075	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0161	0.0104	0.0245	120.1900	0.0100	0.0437	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9911	0.7317	1.3229	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0883	0.0603	0.1269	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6404	1.2343	2.1508	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2746	0.1953	0.3797	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0046	0.0040	0.0042	134.4326	0.9866	0.8691	189.60	
Xylene (-m)						0.0734	0.0499	0.1058	106.1700	0.0029	0.0577	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	May	60.08	48.11	72.06	48.46	0.0065	0.0043	0.0096	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0205	0.0125	0.0327	120.1900	0.0100	0.0456	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1705	0.8318	1.6167	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1088	0.0709	0.1632	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9175	1.3919	2.5963	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3310	0.2255	0.4756	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0056	0.0048	0.0050	134.4755	0.9866	0.8667	189.60	
Xylene (-m)						0.0906	0.0588	0.1364	106.1700	0.0029	0.0585	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jun	64.97	52.07	77.87	48.46	0.0076	0.0050	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0249	0.0148	0.0406	120.1900	0.0100	0.0472	120.19	Option 2: A=7.04383, B=1573.267, C=208.56

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Liquid Contents of Storage Tank - (Continued)

Benzene						1.3383	0.9333	1.8792	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1288	0.0819	0.1970	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.1743	1.5506	2.9903	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3847	0.2567	0.5631	92.1300	0.0003	0.0233	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0065	0.0056	0.0058	134.5075	0.9866	0.8648	189.60	
Xylene (-m)						0.1074	0.0680	0.1651	106.1700	0.0029	0.0591	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jul	67.56	54.78	80.34	48.46	0.0083	0.0054	0.0124	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0275	0.0165	0.0444	120.1900	0.0100	0.0480	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.4350	1.0086	2.0008	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1405	0.0903	0.2131	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.3214	1.6676	3.1718	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.4160	0.2800	0.6042	92.1300	0.0003	0.0232	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0071	0.0061	0.0063	134.5233	0.9866	0.8638	189.60	
Xylene (-m)						0.1173	0.0750	0.1787	106.1700	0.0029	0.0594	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Aug	65.85	54.11	77.60	48.46	0.0078	0.0053	0.0114	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0257	0.0161	0.0402	120.1900	0.0100	0.0475	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.3707	0.9897	1.8660	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1327	0.0882	0.1953	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.2237	1.6382	2.9706	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3952	0.2741	0.5587	92.1300	0.0003	0.0233	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0067	0.0058	0.0061	134.5130	0.9866	0.8644	189.60	
Xylene (-m)						0.1107	0.0733	0.1636	106.1700	0.0029	0.0592	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Sep	60.36	50.29	70.42	48.46	0.0066	0.0047	0.0091	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0207	0.0137	0.0307	120.1900	0.0100	0.0457	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1795	0.8866	1.5486	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1099	0.0768	0.1546	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9313	1.4777	2.4935	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3338	0.2423	0.4532	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0056	0.0049	0.0052	134.4774	0.9866	0.8666	189.60	
Xylene (-m)						0.0915	0.0637	0.1292	106.1700	0.0029	0.0585	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Oct	53.46	45.37	61.54	48.46	0.0052	0.0039	0.0068	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0157	0.0111	0.0217	120.1900	0.0100	0.0435	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9713	0.7673	1.2187	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0861	0.0640	0.1145	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6097	1.2904	1.9915	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2684	0.2060	0.3463	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0045	0.0040	0.0042	134.4272	0.9866	0.8694	189.60	
Xylene (-m)						0.0715	0.0530	0.0954	106.1700	0.0029	0.0576	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Nov	47.24	41.53	52.95	48.46	0.0042	0.0034	0.0051	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0120	0.0094	0.0153	120.1900	0.0100	0.0414	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8108	0.6836	0.9572	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0686	0.0554	0.0845	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3589	1.1581	1.5877	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2191	0.1809	0.2640	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0036	0.0033	0.0035	134.3765	0.9866	0.8721	189.60	
Xylene (-m)						0.0569	0.0458	0.0702	106.1700	0.0029	0.0567	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Dec	41.35	35.95	46.74	48.46	0.0034	0.0031	0.0041	130.0000			188.00	Option 5: A=12.101, B=8907

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Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

1,2,4-Trimethylbenzene	0.0093	0.0073	0.0118	120.1900	0.0100	0.0394	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene	0.6799	0.5760	0.7990	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene	0.0550	0.0446	0.0674	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)	1.1522	0.9865	1.3404	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene	0.1798	0.1492	0.2156	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components	0.0030	0.0027	0.0028	134.3238	0.9866	0.8748	189.60	
Xylene (-m)	0.0455	0.0368	0.0558	106.1700	0.0029	0.0557	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	19.2414	24.2811	37.0200	50.2530	71.2912	85.5226	94.1939	82.4631	58.4532	39.6045	22.4251	18.2242
Vapor Space Volume (cu ft):	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001
Vapor Space Expansion Factor:	0.0501	0.0619	0.0699	0.0811	0.0925	0.0988	0.0974	0.0898	0.0777	0.0632	0.0452	0.0431
Vented Vapor Saturation Factor:	0.9966	0.9961	0.9952	0.9941	0.9928	0.9916	0.9908	0.9913	0.9927	0.9942	0.9953	0.9962
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634	165,260.8634
Tank Diameter (ft):	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000
Vapor Space Outage (ft):	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000
Roof Outage (ft):	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417
Roof Outage (Cone Roof)												
Roof Outage (ft):	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417	1.0417
Roof Height (ft):	3.1250	3.1250	3.1250	3.1250	3.1250	3.1250	3.1250	3.1250	3.1250	3.1250	3.1250	3.1250
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000	50.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Daily Avg. Liquid Surface Temp. (deg. R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Average Ambient Temp. (deg. F):	20.8500	23.3000	32.9500	43.2000	53.3000	62.4000	68.5500	67.2500	59.1000	48.5000	38.7000	26.4500
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292
Tank Paint Solar Absorptance (Shell):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Tank Paint Solar Absorptance (Roof):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Daily Total Solar Insulation Factor (Btu/sqft day):	597.1021	888.0387	1,221.4895	1,492.4381	1,767.1939	1,931.5398	1,909.9654	1,698.9809	1,343.3212	927.0629	571.7205	478.7604
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0501	0.0619	0.0699	0.0811	0.0925	0.0988	0.0974	0.0898	0.0777	0.0632	0.0452	0.0431
Daily Vapor Temperature Range (deg. R):	24.9768	31.0203	35.4252	41.5200	47.9034	51.6085	51.1257	46.9646	40.2648	32.3393	22.8376	21.5716
Daily Vapor Pressure Range (psia):	0.0009	0.0015	0.0028	0.0038	0.0052	0.0065	0.0069	0.0060	0.0044	0.0029	0.0017	0.0010
Breather Vent Press. Setting Range(psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0031	0.0031	0.0031	0.0037	0.0043	0.0050	0.0054	0.0053	0.0047	0.0039	0.0034	0.0031
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0040	0.0046	0.0059	0.0075	0.0096	0.0115	0.0124	0.0114	0.0091	0.0068	0.0051	0.0041
Daily Avg. Liquid Surface Temp. (deg R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Min. Liquid Surface Temp. (deg R):	492.9446	494.0746	499.0107	503.4525	507.7767	511.7372	514.4480	513.7829	509.9612	505.0425	501.1970	495.6241
Daily Max. Liquid Surface Temp. (deg R):	505.4330	509.5847	516.7233	524.2125	531.7283	537.5415	540.0109	537.2652	530.0937	521.2121	512.6158	506.4099
Daily Ambient Temp. Range (deg. R):	18.9000	19.6000	16.9000	18.2000	19.8000	20.6000	20.5000	20.3000	20.4000	20.4000	16.6000	17.3000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9966	0.9961	0.9952	0.9941	0.9928	0.9916	0.9908	0.9913	0.9927	0.9942	0.9953	0.9962
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Vapor Space Outage (ft):	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417	21.0417

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Net Throughput (gal/mo.):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Annual Turnovers:	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	39.0000	39.0000	39.0000	39.0000	39.0000	39.0000	39.0000	39.0000	39.0000	39.0000	39.0000	39.0000
Tank Diameter (ft):	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000	100.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	19.2414	24.2811	37.0200	50.2530	71.2912	85.5226	94.1939	82.4631	58.4532	39.6045	22.4251	18.2242

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	0.00	602.97	602.97
1,2,4-Trimethylbenzene	0.00	27.24	27.24
Benzene	0.00	1.27	1.27
Ethylbenzene	0.00	1.89	1.89
Hexane (-n)	0.00	0.26	0.26
Toluene	0.00	14.25	14.25
Unidentified Components	0.00	522.92	522.92
Xylene (-m)	0.00	35.14	35.14

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002011
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Vertical Fixed Roof Tank
Description:	2005 Operations-Not operational during 2005. No emissions during 2005.

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	90.00
Liquid Height (ft):	35.00
Avg. Liquid Height (ft):	20.00
Volume (gallons):	1,680,000.00
Turnovers:	0.00
Net Throughput (gal/yr):	0.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	Gray/Medium
Shell Condition:	Good
Roof Color/Shade:	Gray/Medium
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	2.81
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	0.00
Pressure Settings (psig):	0.00

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	39.52	33.27	45.76	48.46	0.0031	0.0031	0.0040	130.0000			188.00	Option 1: VP40 = .0031
1,2,4-Trimethylbenzene						0.0086	0.0065	0.0113	120.1900	0.0100	0.0402	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6430	0.5296	0.7762	78.1100	0.0000	0.0024	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0512	0.0401	0.0650	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0936	0.9118	1.3045	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1689	0.1358	0.2087	92.1300	0.0003	0.0252	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	0.0024	0.0025	134.4854	0.9866	0.8713	189.60	
Xylene (-m)						0.0424	0.0331	0.0538	106.1700	0.0029	0.0573	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Feb	42.16	34.40	49.91	48.46	0.0035	0.0031	0.0046	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0097	0.0068	0.0135	120.1900	0.0100	0.0397	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6968	0.5487	0.8769	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0567	0.0420	0.0757	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1791	0.9427	1.4626	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1848	0.1413	0.2393	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0030	0.0027	0.0029	134.3313	0.9866	0.8744	189.60	
Xylene (-m)						0.0469	0.0346	0.0628	106.1700	0.0029	0.0558	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Mar	48.20	39.34	57.05	48.46	0.0044	0.0031	0.0059	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0126	0.0085	0.0181	120.1900	0.0100	0.0417	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8340	0.6395	1.0756	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0711	0.0509	0.0979	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3954	1.0881	1.7713	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2262	0.1679	0.3010	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0038	0.0033	0.0035	134.3847	0.9866	0.8717	189.60	
Xylene (-m)						0.0590	0.0421	0.0814	106.1700	0.0029	0.0568	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Apr	54.16	43.78	64.54	48.46	0.0053	0.0037	0.0075	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0161	0.0104	0.0245	120.1900	0.0100	0.0437	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9911	0.7317	1.3229	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0883	0.0603	0.1269	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6404	1.2343	2.1508	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2746	0.1953	0.3797	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0046	0.0040	0.0042	134.4326	0.9866	0.8691	189.60	
Xylene (-m)						0.0734	0.0499	0.1058	106.1700	0.0029	0.0577	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	May	60.08	48.11	72.06	48.46	0.0065	0.0043	0.0096	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0205	0.0125	0.0327	120.1900	0.0100	0.0456	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1705	0.8318	1.6167	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1088	0.0709	0.1632	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9175	1.3919	2.5963	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3310	0.2255	0.4756	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0056	0.0048	0.0050	134.4755	0.9866	0.8667	189.60	
Xylene (-m)						0.0906	0.0588	0.1364	106.1700	0.0029	0.0585	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jun	64.97	52.07	77.87	48.46	0.0076	0.0050	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0249	0.0148	0.0406	120.1900	0.0100	0.0472	120.19	Option 2: A=7.04383, B=1573.267, C=208.56

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Benzene						1.3383	0.9333	1.8792	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1288	0.0819	0.1970	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.1743	1.5506	2.9903	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3847	0.2567	0.5631	92.1300	0.0003	0.0233	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0065	0.0056	0.0058	134.5075	0.9866	0.8648	189.60	
Xylene (-m)						0.1074	0.0680	0.1651	106.1700	0.0029	0.0591	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jul	67.56	54.78	80.34	48.46	0.0083	0.0054	0.0124	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0275	0.0165	0.0444	120.1900	0.0100	0.0480	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.4350	1.0086	2.0008	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1405	0.0903	0.2131	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.3214	1.6676	3.1718	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.4160	0.2800	0.6042	92.1300	0.0003	0.0232	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0071	0.0061	0.0063	134.5233	0.9866	0.8638	189.60	
Xylene (-m)						0.1173	0.0750	0.1787	106.1700	0.0029	0.0594	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Aug	65.85	54.11	77.60	48.46	0.0078	0.0053	0.0114	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0257	0.0161	0.0402	120.1900	0.0100	0.0475	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.3707	0.9897	1.8660	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1327	0.0882	0.1953	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.2237	1.6382	2.9706	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3952	0.2741	0.5587	92.1300	0.0003	0.0233	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0067	0.0058	0.0061	134.5130	0.9866	0.8644	189.60	
Xylene (-m)						0.1107	0.0733	0.1636	106.1700	0.0029	0.0592	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Sep	60.36	50.29	70.42	48.46	0.0066	0.0047	0.0091	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0207	0.0137	0.0307	120.1900	0.0100	0.0457	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1795	0.8866	1.5486	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1099	0.0768	0.1546	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9313	1.4777	2.4935	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3338	0.2423	0.4532	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0056	0.0049	0.0052	134.4774	0.9866	0.8666	189.60	
Xylene (-m)						0.0915	0.0637	0.1292	106.1700	0.0029	0.0585	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Oct	53.46	45.37	61.54	48.46	0.0052	0.0039	0.0068	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0157	0.0111	0.0217	120.1900	0.0100	0.0435	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9713	0.7673	1.2187	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0861	0.0640	0.1145	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6097	1.2904	1.9915	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2684	0.2060	0.3463	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0045	0.0040	0.0042	134.4272	0.9866	0.8694	189.60	
Xylene (-m)						0.0715	0.0530	0.0954	106.1700	0.0029	0.0576	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Nov	47.24	41.53	52.95	48.46	0.0042	0.0034	0.0051	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0120	0.0094	0.0153	120.1900	0.0100	0.0414	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8108	0.6836	0.9572	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0686	0.0554	0.0845	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3589	1.1581	1.5877	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2191	0.1809	0.2640	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0036	0.0033	0.0035	134.3765	0.9866	0.8721	189.60	
Xylene (-m)						0.0569	0.0458	0.0702	106.1700	0.0029	0.0567	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Dec	41.35	35.95	46.74	48.46	0.0034	0.0031	0.0041	130.0000			188.00	Option 5: A=12.101, B=8907

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1,2,4-Trimethylbenzene	0.0093	0.0073	0.0118	120.1900	0.0100	0.0394	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene	0.6799	0.5760	0.7990	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene	0.0550	0.0446	0.0674	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)	1.1522	0.9865	1.3404	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene	0.1798	0.1492	0.2156	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components	0.0030	0.0027	0.0028	134.3238	0.9866	0.8748	189.60	
Xylene (-m)	0.0455	0.0368	0.0558	106.1700	0.0029	0.0557	106.17	Option 2: A=7.009, B=1462.266, C=215.11

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Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	15.5086	19.5707	29.8385	40.5046	57.4620	68.9333	75.9228	66.4673	47.1144	31.9217	18.0748	14.6888
Vapor Space Volume (cu ft):	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001
Vapor Space Expansion Factor:	0.0501	0.0619	0.0699	0.0811	0.0925	0.0988	0.0974	0.0898	0.0777	0.0632	0.0452	0.0431
Vented Vapor Saturation Factor:	0.9966	0.9961	0.9952	0.9941	0.9928	0.9916	0.9909	0.9914	0.9928	0.9943	0.9953	0.9962
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196	133,198.6196
Tank Diameter (ft):	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000
Vapor Space Outage (ft):	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000
Roof Outage (ft):	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375	0.9375
Roof Height (ft):	2.8125	2.8125	2.8125	2.8125	2.8125	2.8125	2.8125	2.8125	2.8125	2.8125	2.8125	2.8125
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000	45.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Daily Avg. Liquid Surface Temp. (deg. R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Average Ambient Temp. (deg. F):	20.8500	23.3000	32.9500	43.2000	53.3000	62.4000	68.5500	67.2500	59.1000	48.5000	38.7000	26.4500
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292
Tank Paint Solar Absorptance (Shell):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Tank Paint Solar Absorptance (Roof):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Daily Total Solar Insulation Factor (Btu/sqft day):	597.1021	888.0387	1,221.4895	1,492.4381	1,767.1939	1,931.5398	1,909.9654	1,698.9809	1,343.3212	927.0629	571.7205	478.7604
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0501	0.0619	0.0699	0.0811	0.0925	0.0988	0.0974	0.0898	0.0777	0.0632	0.0452	0.0431
Daily Vapor Temperature Range (deg. R):	24.9768	31.0203	35.4252	41.5200	47.9034	51.6085	51.1257	46.9646	40.2648	32.3393	22.6376	21.5716
Daily Vapor Pressure Range (psia):	0.0009	0.0015	0.0028	0.0038	0.0052	0.0065	0.0069	0.0060	0.0044	0.0029	0.0017	0.0010
Breather Vent Press. Setting Range(psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0031	0.0031	0.0031	0.0037	0.0043	0.0050	0.0054	0.0053	0.0047	0.0039	0.0034	0.0031
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0040	0.0046	0.0059	0.0075	0.0096	0.0115	0.0124	0.0114	0.0091	0.0068	0.0051	0.0041
Daily Avg. Liquid Surface Temp. (deg R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Min. Liquid Surface Temp. (deg R):	492.9446	494.0746	499.0107	503.4525	507.7767	511.7372	514.4480	513.7829	509.9612	505.0425	501.1970	495.6241
Daily Max. Liquid Surface Temp. (deg R):	505.4330	509.5847	516.7233	524.2125	531.7283	537.5415	540.0109	537.2652	530.0937	521.2121	512.6158	506.4099
Daily Ambient Temp. Range (deg. R):	18.9000	19.6000	16.9000	18.2000	19.8000	20.6000	20.5000	20.3000	20.4000	20.4000	16.6000	17.3000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9966	0.9961	0.9952	0.9941	0.9928	0.9916	0.9909	0.9914	0.9928	0.9943	0.9953	0.9962
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Vapor Space Outage (ft):	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375	20.9375

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Net Throughput (gal/mo.):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Annual Turnovers:	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000	1,680,000.000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	35.0000	35.0000	35.0000	35.0000	35.0000	35.0000	35.0000	35.0000	35.0000	35.0000	35.0000	35.0000
Tank Diameter (ft):	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000	90.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	15.5086	19.5707	29.8385	40.5046	57.4620	68.9333	75.9228	66.4673	47.1144	31.9217	18.0748	14.6888

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	0.00	486.01	486.01
1,2,4-Trimethylbenzene	0.00	21.95	21.95
Benzene	0.00	1.02	1.02
Ethylbenzene	0.00	1.53	1.53
Hexane (-n)	0.00	0.21	0.21
Toluene	0.00	11.49	11.49
Unidentified Components	0.00	421.48	421.48
Xylene (-m)	0.00	28.33	28.33

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002012
City:	Searsport
State:	Maine
Company:	Irving Oil Corp.
Type of Tank:	Vertical Fixed Roof Tank
Description:	2005 Operations-Not operational during 2005. No emissions from this tank during 2005.

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	80.00
Liquid Height (ft):	20.00
Avg. Liquid Height (ft):	10.00
Volume (gallons):	756,000.00
Turnovers:	0.00
Net Throughput (gal/yr):	0.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	Gray/Medium
Shell Condition:	Good
Roof Color/Shade:	Gray/Medium
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	0.00
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	0.00
Pressure Settings (psig):	0.00

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Jet kerosene	Jan	39.52	33.27	45.76	48.46	0.0041	0.0041	0.0051	130.0000			162.00	Option 1: VP40 = .0041
Benzene						0.6430	0.5296	0.7762	78.1100	0.0000	0.0078	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0512	0.0401	0.0650	106.1700	0.0013	0.0198	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0936	0.9118	1.3045	86.1700	0.0001	0.0166	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1689	0.1358	0.2087	92.1300	0.0013	0.0683	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0033	0.0029	0.0031	139.0409	0.9942	0.8476	162.55	
Xylene (-m)						0.0424	0.0331	0.0538	106.1700	0.0031	0.0399	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Feb	42.16	34.40	49.91	48.46	0.0045	0.0041	0.0059	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.6968	0.5487	0.8769	78.1100	0.0000	0.0078	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0567	0.0420	0.0757	106.1700	0.0013	0.0201	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1791	0.9427	1.4626	86.1700	0.0001	0.0164	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1848	0.1413	0.2393	92.1300	0.0013	0.0686	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0036	0.0031	0.0033	139.0907	0.9942	0.8466	162.55	
Xylene (-m)						0.0469	0.0346	0.0628	106.1700	0.0031	0.0406	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Mar	48.20	39.34	57.05	48.46	0.0055	0.0041	0.0075	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.8340	0.6395	1.0756	78.1100	0.0000	0.0075	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0711	0.0509	0.0979	106.1700	0.0013	0.0204	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3954	1.0881	1.7713	86.1700	0.0001	0.0157	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2262	0.1679	0.3010	92.1300	0.0013	0.0679	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0044	0.0038	0.0040	138.9839	0.9942	0.8472	162.55	
Xylene (-m)						0.0590	0.0421	0.0814	106.1700	0.0031	0.0413	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Apr	54.16	43.78	64.54	48.46	0.0068	0.0047	0.0096	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.9911	0.7317	1.3229	78.1100	0.0000	0.0073	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0883	0.0603	0.1269	106.1700	0.0013	0.0206	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6404	1.2343	2.1508	86.1700	0.0001	0.0151	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2746	0.1953	0.3797	92.1300	0.0013	0.0672	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0054	0.0046	0.0049	138.8737	0.9942	0.8479	162.55	
Xylene (-m)						0.0734	0.0499	0.1058	106.1700	0.0031	0.0419	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	May	60.08	48.11	72.06	48.46	0.0083	0.0055	0.0122	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						1.1705	0.8318	1.6167	78.1100	0.0000	0.0071	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1088	0.0709	0.1632	106.1700	0.0013	0.0209	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9175	1.3919	2.5963	86.1700	0.0001	0.0145	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3310	0.2255	0.4756	92.1300	0.0013	0.0665	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0066	0.0056	0.0059	138.7604	0.9942	0.8487	162.55	
Xylene (-m)						0.0906	0.0588	0.1364	106.1700	0.0031	0.0424	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Jun	64.97	52.07	77.87	48.46	0.0097	0.0063	0.0146	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						1.3383	0.9333	1.8792	78.1100	0.0000	0.0069	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1288	0.0819	0.1970	106.1700	0.0013	0.0210	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.1743	1.5506	2.9903	86.1700	0.0001	0.0140	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3847	0.2567	0.5631	92.1300	0.0013	0.0658	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0078	0.0065	0.0068	138.6644	0.9942	0.8494	162.55	
Xylene (-m)						0.1074	0.0680	0.1651	106.1700	0.0031	0.0428	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Jul	67.56	54.78	80.34	48.46	0.0105	0.0069	0.0157	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						1.4350	1.0086	2.0008	78.1100	0.0000	0.0068	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1405	0.0903	0.2131	106.1700	0.0013	0.0211	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.3214	1.6676	3.1718	86.1700	0.0001	0.0137	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.4160	0.2800	0.6042	92.1300	0.0013	0.0655	92.13	Option 2: A=6.954, B=1344.8, C=219.48

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Unidentified Components						0.0085	0.0071	0.0075	138.6128	0.9942	0.8499	162.55	
Xylene (-m)						0.1173	0.0750	0.1787	106.1700	0.0031	0.0430	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Aug	65.85	54.11	77.60	48.46	0.0100	0.0068	0.0145	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						1.3707	0.9897	1.8660	78.1100	0.0000	0.0069	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1327	0.0882	0.1953	106.1700	0.0013	0.0211	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.2237	1.6382	2.9706	86.1700	0.0001	0.0139	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3952	0.2741	0.5587	92.1300	0.0013	0.0657	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0080	0.0068	0.0071	138.6468	0.9942	0.8496	162.55	
Xylene (-m)						0.1107	0.0733	0.1636	106.1700	0.0031	0.0429	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Sep	60.36	50.29	70.42	48.46	0.0083	0.0059	0.0115	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						1.1795	0.8866	1.5486	78.1100	0.0000	0.0071	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1099	0.0768	0.1546	106.1700	0.0013	0.0209	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9313	1.4777	2.4935	86.1700	0.0001	0.0144	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3338	0.2423	0.4532	92.1300	0.0013	0.0664	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0067	0.0057	0.0061	138.7551	0.9942	0.8487	162.55	
Xylene (-m)						0.0915	0.0637	0.1292	106.1700	0.0031	0.0424	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Oct	53.46	45.37	61.54	48.46	0.0066	0.0050	0.0087	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.9713	0.7673	1.2187	78.1100	0.0000	0.0073	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0861	0.0640	0.1145	106.1700	0.0013	0.0206	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6097	1.2904	1.9915	86.1700	0.0001	0.0152	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2684	0.2060	0.3463	92.1300	0.0013	0.0673	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0053	0.0046	0.0049	138.8869	0.9942	0.8478	162.55	
Xylene (-m)						0.0715	0.0530	0.0954	106.1700	0.0031	0.0418	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Nov	47.24	41.53	52.95	48.46	0.0053	0.0044	0.0065	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.8108	0.6836	0.9572	78.1100	0.0000	0.0076	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0686	0.0554	0.0845	106.1700	0.0013	0.0203	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3589	1.1581	1.5877	86.1700	0.0001	0.0159	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2191	0.1809	0.2640	92.1300	0.0013	0.0680	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0043	0.0038	0.0040	139.0012	0.9942	0.8471	162.55	
Xylene (-m)						0.0569	0.0458	0.0702	106.1700	0.0031	0.0412	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Jet kerosene	Dec	41.35	35.95	46.74	48.46	0.0043	0.0041	0.0052	130.0000			162.00	Option 5: A=12.39, B=8933
Benzene						0.6799	0.5760	0.7990	78.1100	0.0000	0.0078	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0550	0.0446	0.0674	106.1700	0.0013	0.0200	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1522	0.9865	1.3404	86.1700	0.0001	0.0165	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1798	0.1492	0.2156	92.1300	0.0013	0.0687	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0035	0.0031	0.0033	139.1047	0.9942	0.8465	162.55	
Xylene (-m)						0.0455	0.0368	0.0558	106.1700	0.0031	0.0405	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	23.7914	28.7779	43.8818	59.5651	84.4728	101.2929	111.5317	97.6598	69.2593	46.9446	26.5858	21.5976
Vapor Space Volume (cu ft):	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001
Vapor Space Expansion Factor:	0.0501	0.0619	0.0700	0.0811	0.0926	0.0989	0.0976	0.0899	0.0778	0.0633	0.0452	0.0431
Vented Vapor Saturation Factor:	0.9933	0.9928	0.9911	0.9891	0.9867	0.9844	0.9831	0.9840	0.9866	0.9893	0.9913	0.9930
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374	154,985.2374
Tank Diameter (ft):	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000
Vapor Space Outage (ft):	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000	10.0000
Roof Outage (ft):	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333
Roof Outage (Cone Roof)												
Roof Outage (ft):	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333	0.8333
Roof Height (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0041	0.0045	0.0055	0.0068	0.0083	0.0097	0.0105	0.0100	0.0083	0.0066	0.0053	0.0043
Daily Avg. Liquid Surface Temp. (deg. R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Average Ambient Temp. (deg. F):	20.8500	23.3000	32.9500	43.2000	53.3000	62.4000	68.5500	67.2500	59.1000	48.5000	38.7000	26.4500
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292
Tank Paint Solar Absorptance (Shell):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Tank Paint Solar Absorptance (Roof):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Daily Total Solar Insulation Factor (Btu/sqft day):	597.1021	888.0387	1,221.4895	1,492.4381	1,767.1939	1,931.5398	1,909.9654	1,698.9809	1,343.3212	927.0629	571.7205	478.7604
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0501	0.0619	0.0700	0.0811	0.0926	0.0989	0.0976	0.0899	0.0778	0.0633	0.0452	0.0431
Daily Vapor Temperature Range (deg. R):	24.9768	31.0203	35.4252	41.5200	47.9034	51.6085	51.1257	46.9646	40.2648	32.3393	22.8376	21.5716
Daily Vapor Pressure Range (psia):	0.0010	0.0018	0.0034	0.0048	0.0067	0.0083	0.0088	0.0077	0.0056	0.0037	0.0021	0.0011
Breather Vent Press. Setting Range(psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0041	0.0045	0.0055	0.0068	0.0083	0.0097	0.0105	0.0100	0.0083	0.0066	0.0053	0.0043
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0041	0.0041	0.0041	0.0047	0.0055	0.0063	0.0069	0.0068	0.0059	0.0050	0.0044	0.0041
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0051	0.0059	0.0075	0.0096	0.0122	0.0146	0.0157	0.0145	0.0115	0.0087	0.0065	0.0052
Daily Avg. Liquid Surface Temp. (deg R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Min. Liquid Surface Temp. (deg R):	492.9446	494.0746	499.0107	503.4525	507.7767	511.7372	514.4480	513.7829	509.9612	505.0425	501.1970	495.6241
Daily Max. Liquid Surface Temp. (deg R):	505.4330	509.5847	516.7233	524.2125	531.7283	537.5415	540.0109	537.2652	530.0937	521.2121	512.6158	506.4099
Daily Ambient Temp. Range (deg. R):	18.9000	19.6000	16.9000	18.2000	19.8000	20.6000	20.5000	20.3000	20.4000	20.4000	16.6000	17.3000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9933	0.9928	0.9911	0.9891	0.9867	0.9844	0.9831	0.9840	0.9866	0.9893	0.9913	0.9930
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0041	0.0045	0.0055	0.0068	0.0083	0.0097	0.0105	0.0100	0.0083	0.0066	0.0053	0.0043
Vapor Space Outage (ft):	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333	30.8333

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0041	0.0045	0.0055	0.0068	0.0083	0.0097	0.0105	0.0100	0.0083	0.0066	0.0053	0.0043
Net Throughput (gal/mo.):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Annual Turnovers:	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	756,000.0000	756,000.0000	756,000.0000	756,000.0000	756,000.0000	756,000.0000	756,000.0000	756,000.0000	756,000.0000	756,000.0000	756,000.0000	756,000.0000
Maximum Liquid Height (ft):	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000
Tank Diameter (ft):	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000	80.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	23.7914	28.7779	43.8818	59.5651	84.4728	101.2929	111.5317	97.6598	69.2593	46.9446	26.5858	21.5976

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Jet kerosene	0.00	715.36	715.36
Benzene	0.00	5.10	5.10
Ethylbenzene	0.00	14.87	14.87
Hexane (-n)	0.00	10.48	10.48
Toluene	0.00	47.63	47.63
Unidentified Components	0.00	607.08	607.08
Xylene (-m)	0.00	30.20	30.20

TANKS 4.0
Emissions Report - Detail Format
Tank Identification and Physical Characteristics

Identification

User Identification:	1183002013
City:	Searsport
State:	Maine
Company:	Irving Oil Corp
Type of Tank:	Vertical Fixed Roof Tank
Description:	2005 Operations-Not operational during 2005. No emissions during 2005.

Tank Dimensions

Shell Height (ft):	40.00
Diameter (ft):	110.00
Liquid Height (ft):	30.00
Avg. Liquid Height (ft):	20.00
Volume (gallons):	2,100,000.00
Turnovers:	0.00
Net Throughput (gal/yr):	0.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	Gray/Medium
Shell Condition:	Good
Roof Color/Shade:	Gray/Medium
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft):	3.75
Slope (ft/ft) (Cone Roof):	0.06

Breather Vent Settings

Vacuum Settings (psig):	0.00
Pressure Settings (psig):	0.00

Meteorological Data used in Emissions Calculations: Portland, Maine (Avg Atmospheric Pressure = 14.69 psia)

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Mixture/Component	Month	Daily Liquid Surf. Temperatures (deg F) Avg.	Min.	Max.	Liquid Bulk Temp. (deg F)	Vapor Pressures (psia) Avg.	Min.	Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Distillate fuel oil no. 2	Jan	39.52	33.27	45.76	48.46	0.0031	0.0031	0.0040	130.0000			188.00	Option 1: VP40 = .0031
1,2,4-Trimethylbenzene						0.0086	0.0065	0.0113	120.1900	0.0100	0.0402	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6430	0.5296	0.7762	78.1100	0.0000	0.0024	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0512	0.0401	0.0650	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.0936	0.9118	1.3045	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1689	0.1358	0.2087	92.1300	0.0003	0.0252	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0027	0.0024	0.0025	134.4854	0.9866	0.8713	189.60	
Xylene (-m)						0.0424	0.0331	0.0538	106.1700	0.0029	0.0573	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Feb	42.16	34.40	49.91	48.46	0.0035	0.0031	0.0046	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0097	0.0068	0.0135	120.1900	0.0100	0.0397	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.6968	0.5487	0.8769	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0567	0.0420	0.0757	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.1791	0.9427	1.4626	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.1846	0.1413	0.2393	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0030	0.0027	0.0029	134.3313	0.9866	0.8744	189.60	
Xylene (-m)						0.0469	0.0346	0.0628	106.1700	0.0029	0.0558	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Mar	48.20	39.34	57.05	48.46	0.0044	0.0031	0.0059	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0126	0.0085	0.0181	120.1900	0.0100	0.0417	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8340	0.6395	1.0756	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0711	0.0509	0.0979	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3954	1.0881	1.7713	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2262	0.1679	0.3010	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0038	0.0033	0.0035	134.3847	0.9866	0.8717	189.60	
Xylene (-m)						0.0590	0.0421	0.0814	106.1700	0.0029	0.0568	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Apr	54.16	43.78	64.54	48.46	0.0053	0.0037	0.0075	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0161	0.0104	0.0245	120.1900	0.0100	0.0437	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9911	0.7317	1.3229	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0883	0.0603	0.1269	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6404	1.2343	2.1508	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2746	0.1953	0.3797	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0046	0.0040	0.0042	134.4326	0.9866	0.8691	189.60	
Xylene (-m)						0.0734	0.0499	0.1058	106.1700	0.0029	0.0577	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	May	60.08	48.11	72.06	48.46	0.0065	0.0043	0.0096	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0205	0.0125	0.0327	120.1900	0.0100	0.0456	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1705	0.8318	1.6167	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1088	0.0709	0.1632	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9175	1.3919	2.5963	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3310	0.2255	0.4756	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0056	0.0048	0.0050	134.4755	0.9866	0.8667	189.60	
Xylene (-m)						0.0906	0.0588	0.1364	106.1700	0.0029	0.0585	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jun	64.97	52.07	77.87	48.46	0.0076	0.0050	0.0115	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0249	0.0148	0.0406	120.1900	0.0100	0.0472	120.19	Option 2: A=7.04383, B=1573.267, C=208.56

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

Benzene						1.3383	0.9333	1.8792	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1288	0.0819	0.1970	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.1743	1.5506	2.9903	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3847	0.2567	0.5631	92.1300	0.0003	0.0233	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0065	0.0056	0.0058	134.5075	0.9866	0.8648	189.60	
Xylene (-m)						0.1074	0.0680	0.1651	106.1700	0.0029	0.0591	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Jul	67.56	54.78	80.34	48.46	0.0083	0.0054	0.0124	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0275	0.0165	0.0444	120.1900	0.0100	0.0480	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.4350	1.0086	2.0008	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1405	0.0903	0.2131	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.3214	1.6676	3.1718	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.4160	0.2800	0.6042	92.1300	0.0003	0.0232	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0071	0.0061	0.0063	134.5233	0.9866	0.8638	189.60	
Xylene (-m)						0.1173	0.0750	0.1787	106.1700	0.0029	0.0594	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Aug	65.85	54.11	77.60	48.46	0.0078	0.0053	0.0114	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0257	0.0161	0.0402	120.1900	0.0100	0.0475	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.3707	0.9897	1.8660	78.1100	0.0000	0.0020	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1327	0.0882	0.1953	106.1700	0.0001	0.0032	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						2.2237	1.6382	2.9706	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3952	0.2741	0.5587	92.1300	0.0003	0.0233	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0067	0.0058	0.0061	134.5130	0.9866	0.8644	189.60	
Xylene (-m)						0.1107	0.0733	0.1636	106.1700	0.0029	0.0592	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Sep	60.36	50.29	70.42	48.46	0.0066	0.0047	0.0091	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0207	0.0137	0.0307	120.1900	0.0100	0.0457	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						1.1795	0.8866	1.5486	78.1100	0.0000	0.0021	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.1099	0.0768	0.1546	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.9313	1.4777	2.4935	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.3338	0.2423	0.4532	92.1300	0.0003	0.0236	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0056	0.0049	0.0052	134.4774	0.9866	0.8666	189.60	
Xylene (-m)						0.0915	0.0637	0.1292	106.1700	0.0029	0.0585	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Oct	53.46	45.37	61.54	48.46	0.0052	0.0039	0.0068	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0157	0.0111	0.0217	120.1900	0.0100	0.0435	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9713	0.7673	1.2187	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0861	0.0640	0.1145	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.6097	1.2904	1.9915	86.1700	0.0000	0.0004	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2684	0.2060	0.3463	92.1300	0.0003	0.0238	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0045	0.0040	0.0042	134.4272	0.9866	0.8694	189.60	
Xylene (-m)						0.0715	0.0530	0.0954	106.1700	0.0029	0.0576	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Nov	47.24	41.53	52.95	48.46	0.0042	0.0034	0.0051	130.0000			188.00	Option 5: A=12.101, B=8907
1,2,4-Trimethylbenzene						0.0120	0.0094	0.0153	120.1900	0.0100	0.0414	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.8108	0.6836	0.9572	78.1100	0.0000	0.0022	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0686	0.0554	0.0845	106.1700	0.0001	0.0031	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)						1.3589	1.1581	1.5877	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene						0.2191	0.1809	0.2640	92.1300	0.0003	0.0241	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components						0.0036	0.0033	0.0035	134.3765	0.9866	0.8721	189.60	
Xylene (-m)						0.0569	0.0458	0.0702	106.1700	0.0029	0.0567	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Distillate fuel oil no. 2	Dec	41.35	35.95	46.74	48.46	0.0034	0.0031	0.0041	130.0000			188.00	Option 5: A=12.101, B=8907

TANKS 4.0
Emissions Report - Detail Format
Liquid Contents of Storage Tank - (Continued)

1,2,4-Trimethylbenzene	0.0093	0.0073	0.0118	120.1900	0.0100	0.0394	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene	0.6799	0.5760	0.7990	78.1100	0.0000	0.0023	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene	0.0550	0.0446	0.0674	106.1700	0.0001	0.0030	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Hexane (-n)	1.1522	0.9865	1.3404	86.1700	0.0000	0.0005	86.17	Option 2: A=6.876, B=1171.17, C=224.41
Toluene	0.1798	0.1492	0.2156	92.1300	0.0003	0.0243	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Unidentified Components	0.0030	0.0027	0.0028	134.3238	0.9866	0.8748	189.60	
Xylene (-m)	0.0455	0.0368	0.0558	106.1700	0.0029	0.0557	106.17	Option 2: A=7.009, B=1462.266, C=215.11

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (lb):	23.5118	29.6699	45.2356	61.4045	87.1102	104.4982	115.0926	100.7596	71.4235	48.3931	27.4018	22.2688
Vapor Space Volume (cu ft):	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001
Vapor Space Expansion Factor:	0.0501	0.0619	0.0699	0.0811	0.0925	0.0988	0.0974	0.0898	0.0777	0.0632	0.0452	0.0431
Vented Vapor Saturation Factor:	0.9965	0.9960	0.9951	0.9940	0.9927	0.9915	0.9908	0.9912	0.9927	0.9942	0.9953	0.9962
Tank Vapor Space Volume												
Vapor Space Volume (cu ft):	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025	201,945.5025
Tank Diameter (ft):	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000
Vapor Space Outage (ft):	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500
Tank Shell Height (ft):	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000	40.0000
Average Liquid Height (ft):	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000	20.0000
Roof Outage (ft):	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500
Roof Outage (Cone Roof)												
Roof Outage (ft):	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500	1.2500
Roof Height (ft):	3.7500	3.7500	3.7500	3.7500	3.7500	3.7500	3.7500	3.7500	3.7500	3.7500	3.7500	3.7500
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625
Shell Radius (ft):	55.0000	55.0000	55.0000	55.0000	55.0000	55.0000	55.0000	55.0000	55.0000	55.0000	55.0000	55.0000
Vapor Density												
Vapor Density (lb/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Daily Avg. Liquid Surface Temp. (deg. R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Average Ambient Temp. (deg. F):	20.8500	23.3000	32.9500	43.2000	53.3000	62.4000	68.5500	67.2500	59.1000	48.5000	38.7000	26.4500
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292	508.1292
Tank Paint Solar Absorptance (Shell):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Tank Paint Solar Absorptance (Roof):	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800	0.6800
Daily Total Solar Insulation Factor (Btu/sqft day):	597.1021	888.0387	1,221.4895	1,492.4381	1,767.1939	1,931.5398	1,909.9654	1,698.9809	1,343.3212	927.0629	571.7205	478.7604
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:	0.0501	0.0619	0.0699	0.0811	0.0925	0.0988	0.0974	0.0898	0.0777	0.0632	0.0452	0.0431
Daily Vapor Temperature Range (deg. R):	24.9768	31.0203	35.4252	41.5200	47.9034	51.6085	51.1257	46.9646	40.2648	32.3393	22.8376	21.5716
Daily Vapor Pressure Range (psia):	0.0009	0.0015	0.0028	0.0038	0.0052	0.0065	0.0069	0.0060	0.0044	0.0029	0.0017	0.0010
Breather Vent Press. Setting Range(psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.0031	0.0031	0.0031	0.0037	0.0043	0.0050	0.0054	0.0053	0.0047	0.0039	0.0034	0.0031
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.0040	0.0046	0.0059	0.0075	0.0096	0.0115	0.0124	0.0114	0.0091	0.0068	0.0051	0.0041
Daily Avg. Liquid Surface Temp. (deg R):	499.1888	501.8297	507.8670	513.8325	519.7525	524.6394	527.2295	525.5241	520.0275	513.1273	506.9064	501.0170
Daily Min. Liquid Surface Temp. (deg R):	492.9446	494.0746	499.0107	503.4525	507.7767	511.7372	514.4480	513.7829	509.9612	505.0425	501.1970	495.6241
Daily Max. Liquid Surface Temp. (deg R):	505.4330	509.5847	516.7233	524.2125	531.7283	537.5415	540.0109	537.2652	530.0937	521.2121	512.6158	506.4099
Daily Ambient Temp. Range (deg. R):	18.9000	19.6000	16.9000	18.2000	19.8000	20.6000	20.5000	20.3000	20.4000	20.4000	16.6000	17.3000
Vented Vapor Saturation Factor												
Vented Vapor Saturation Factor:	0.9965	0.9960	0.9951	0.9940	0.9927	0.9915	0.9908	0.9912	0.9927	0.9942	0.9953	0.9962
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Vapor Space Outage (ft):	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500	21.2500

TANKS 4.0
Emissions Report - Detail Format
Detail Calculations (AP-42)- (Continued)

Working Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (lb/lb-mole):	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000	130.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0031	0.0035	0.0044	0.0053	0.0065	0.0076	0.0083	0.0078	0.0066	0.0052	0.0042	0.0034
Net Throughput (gal/mo.):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Annual Turnovers:	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Turnover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Maximum Liquid Volume (gal):	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000	2,100,000.000
	0	0	0	0	0	0	0	0	0	0	0	0
Maximum Liquid Height (ft):	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000	30.0000
Tank Diameter (ft):	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000	110.0000
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	23.5118	29.6699	45.2356	61.4045	87.1102	104.4982	115.0926	100.7596	71.4235	48.3931	27.4018	22.2688

TANKS 4.0
Emissions Report - Detail Format
Individual Tank Emission Totals

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	0.00	736.77	736.77
1,2,4-Trimethylbenzene	0.00	33.28	33.28
Benzene	0.00	1.55	1.55
Ethylbenzene	0.00	2.31	2.31
Hexane (-n)	0.00	0.32	0.32
Toluene	0.00	17.42	17.42
Unidentified Components	0.00	638.95	638.95
Xylene (-m)	0.00	42.94	42.94

TANKS 4.0
Emissions Report - Detail Format
Total Emissions Summaries - All Tanks in Report

Emissions Report for: January , February , March , April , May , June , July , August , September , October , November , December

Tank Identification				Losses (lbs)
1183002001.tn	Irving Oil Corp	Internal Floating Roof Tank	Searsport, Maine	11,522.23
1183002002	Irving Oil Corp	Internal Floating Roof Tank	Searsport, Maine	140.24
1183002003	Irving Oil Corp	Internal Floating Roof Tank	Searsport, Maine	26.55
1183002004	Irving Oil Corp	Vertical Fixed Roof Tank	Searsport, Maine	18.73
1183002005.tn	Irving Oil Corp.	Internal Floating Roof Tank	Searsport, Maine	7,398.13
1183002006.tn	Irving Oil Corp	Internal Floating Roof Tank	Searsport, Maine	107.55
1183002007-A	Irving Oil Corp	Internal Floating Roof Tank	Searsport, Maine	31.92
1183002008-B	Irving Oil Corp	Internal Floating Roof Tank	Searsport, Maine	50.89
1183002009	Irving Oil Corp	Vertical Fixed Roof Tank	Searsport, Maine	1,205.06
1183002010	Irving Oil Corp	Vertical Fixed Roof Tank	Searsport, Maine	602.97
1183002011	Irving Oil Corp	Vertical Fixed Roof Tank	Searsport, Maine	486.01
1183002012	Irving Oil Corp.	Vertical Fixed Roof Tank	Searsport, Maine	715.36
1183002013	Irving Oil Corp	Vertical Fixed Roof Tank	Searsport, Maine	736.77
Total Emissions for all Tanks:				23,042.42

ATTACHMENT 3

PUBLIC NOTICE OF INTENT TO FILE

PUBLIC NOTICE OF INTENT TO FILE

Please take notice that Irving Oil Terminals, Inc., 52 Station Avenue, Searsport, ME 04974, Tel: 207-548-2501, intends to file an Air Emission License application with the Maine Department of Environmental Protection (DEP) pursuant to the provisions of 38 M.R.S.A., Section 590 on February 12, 2007. The application is for renewal of their existing air emission license which permits emissions associated with the bulk storage of petroleum products and associated operations of their terminal located in Searsport, Maine. According to Department regulations, interested parties must be publicly notified, written comments invited, and if justified, an opportunity for public hearing given. A request for a public hearing or for the Board of Environmental Protection to assume jurisdiction must be received by the Department, in writing, no later than 20 days after the application is accepted by the Department as complete for processing. The application and supporting documentation will be available for review at the Bureau of Air Quality (BAQ) DEP office in Augusta, (207) 287-2437, during normal working hours. A copy of the application and supporting documentation will also be available at the municipal office in Searsport, Maine. Written public comments may be sent to Mark Roberts at the Bureau of Air Quality, 17 State House Station, Augusta, Maine 04333-0017.

Published Feb. 10, 2007
Waldo Independent

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ATTACHMENT #4

CALCULATIONS

The following provides the emission calculations for Boiler #2 and Generator #1. Emission factors are based on those listed in previous licensing actions.

Boiler #2

Maximum Design Capacity = 1.68 MMBtu/hr
Maximum Firing Rate = 12 gal/hr
Fuel Type = #2 fuel oil at 0.35% sulfur
Maximum Licensed Fuel Usage = 20,000 gal/yr
Maximum Annual Operational Hours - Limited Maximum Licensed Fuel Usage
PM Emission Factor = 0.17 lb/hr
PM_{10} Emission Factor = 0.17 lb/hr
SO_2 Emission Factor = 0.60 lb/hr
NO_X Emission Factor = 0.84 lb/hr
CO Emission Factor = 0.06 lb/hr
VOC Emission Factor = 0.01 lb/hr

Total hours of usage boiler can operate based on a 20,000 gal/yr fuel restriction:

(20,000 gal/yr)/(12 gal/hr) = 1,666.67 hr/yr

Total annual maximum emissions based on operating boiler for 1,666.67 hr/yr-numbers rounded to the nearest hundredth:

Annual PM emissions = (0.17 lb/hr) x (1,666.67 hr/yr) = 283.33 lb/yr = **0.14 ton/yr**
Annual PM_{10} emissions = (0.17 lb/hr) x (1,666.67 hr/yr) = 283.33 lb/yr = **0.14 ton/yr**
Annual SO_2 emissions = (0.60 lb/hr) x (1,666.67 hr/yr) = 1,000.00 lb/yr = **0.50 ton/yr**
Annual NO_X emissions = (0.84 lb/hr) x (1,666.67 hr/yr) = 1,400.00 lb/yr = **0.70 ton/yr**
Annual CO emissions = (0.06 lb/hr) x (1,666.67 hr/yr) = 100.00 lb/yr = **0.05 ton/yr**
Annual VOC emissions = (0.01 lb/hr) x (1,666.67 hr/yr) = 16.67 lb/yr = **0.01 ton/yr**

Generator #1

Maximum Design Capacity = 0.7 MMBtu/hr
Maximum Firing Rate = 7.4 gal/hr
Fuel Type = Propane
Power Output = 70 kW
Maximum Annual Operational Hours = 500 hr/yr
PM Emission Factor = 0.10 lb/hr
PM_{10} Emission Factor = 0.10 lb/hr

SO_2 Emission Factor = 0.05 lb/hr
NO_X Emission Factor = 4.54 lb/hr
CO Emission Factor = 0.98 lb/hr
VOC Emission Factor = 0.36 lb/hr

Total annual maximum emissions based on operating generator for 500 hr/yr-numbers rounded to the nearest hundredth:

Annual PM emissions = (0.10 lb/hr) x (500 hr/yr) = 50.00 lb/yr = **0.03 ton/yr**
Annual PM_{10} emissions = (0.10 lb/hr) x (500 hr/yr) = 50.00 lb/yr = **0.03 ton/yr**
Annual SO_2 emissions = (0.05 lb/hr) x (500 hr/yr) = 25.00 lb/yr = **0.01 ton/yr**
Annual NO_X emissions = (4.54 lb/hr) x (500 hr/yr) = 2,270.00 lb/yr = **1.14 ton/yr***
Annual CO emissions = (0.98 lb/hr) x (500 hr/yr) = 490.00 lb/yr = **0.25 ton/yr**
Annual VOC emissions = (0.36 lb/hr) x (500 hr/yr) = 180.00 lb/yr = **0.09 ton/yr**

*Based on the current license amendment (A-413-71-G-A) the total allowable annual NO_X emissions for Generator #1 is 0.6 ton/yr. Based on above calculation, Irving Oil is requesting that this be revised to reflect 1.14 ton/yr in this license renewal.

Total 2005 Emissions

The following table provides a summary of the total 2005 emissions at the Irving Oil Searsport facility and compares them to the currently licensed emission limits.

Total 2005 Emissions (Tons)									Licensed Emissions (Tons)
Pollutant	Boiler #1	Boiler #2*	Generator #1*	Loading Racks	Storage Tanks	Ballasting	Equip Leaks	Total	Total
PM	-	0.14	0.03	-	-	-	-	0.17	3.0
PM_{10}	-	0.14	0.03	-	-	-	-	0.17	3.0
SO_2	-	0.50	0.01	-	-	-	-	0.51	32.0
NO_X	-	0.70	1.14	-	-	-	-	1.84	8.3
CO	-	0.05	0.25	-	-	-	-	0.3	0.7
VOC	-	0.01	0.09	5.65	8.56	-	0.10	14.41	49.9

*Total emissions are based on maximum permitted operations.